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COMSOL  
CONFERENCE  
2015 BOSTON

# Understanding the Transition Flow region through COMSOL Multiphysics modeling

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## ➤ Background

- Scale in Flow Modeling
- Knudsen Number and Flow Equations
- Influences at Different Scale
- Different Approaches to Modeling Transition Flow

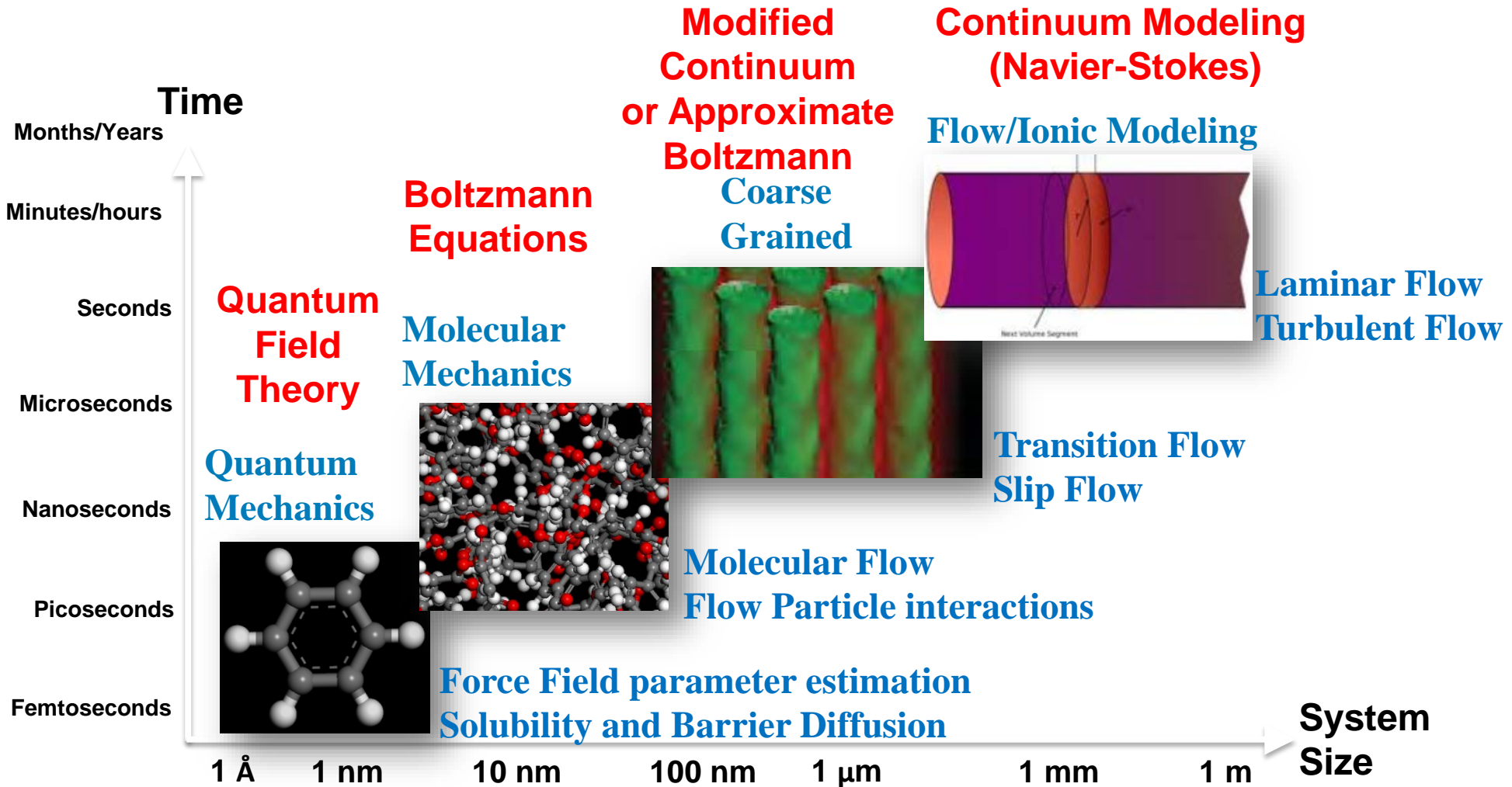
## ➤ Examples of Modeling Transition Flow of Gases

- Higher Order Slip Flow
  - » Flow profile – pressure dependence (first order and second order slip approximation)
  - » Validating the model through standard flow (helium and nitrogen)
  - » Variation of Knudsen flow along the pore
- Self Diffusion modification of Navier Stokes Equation
- Example of binary flow

## ➤ Summary

## ➤ Other Approaches

# Scales in Flow Modeling

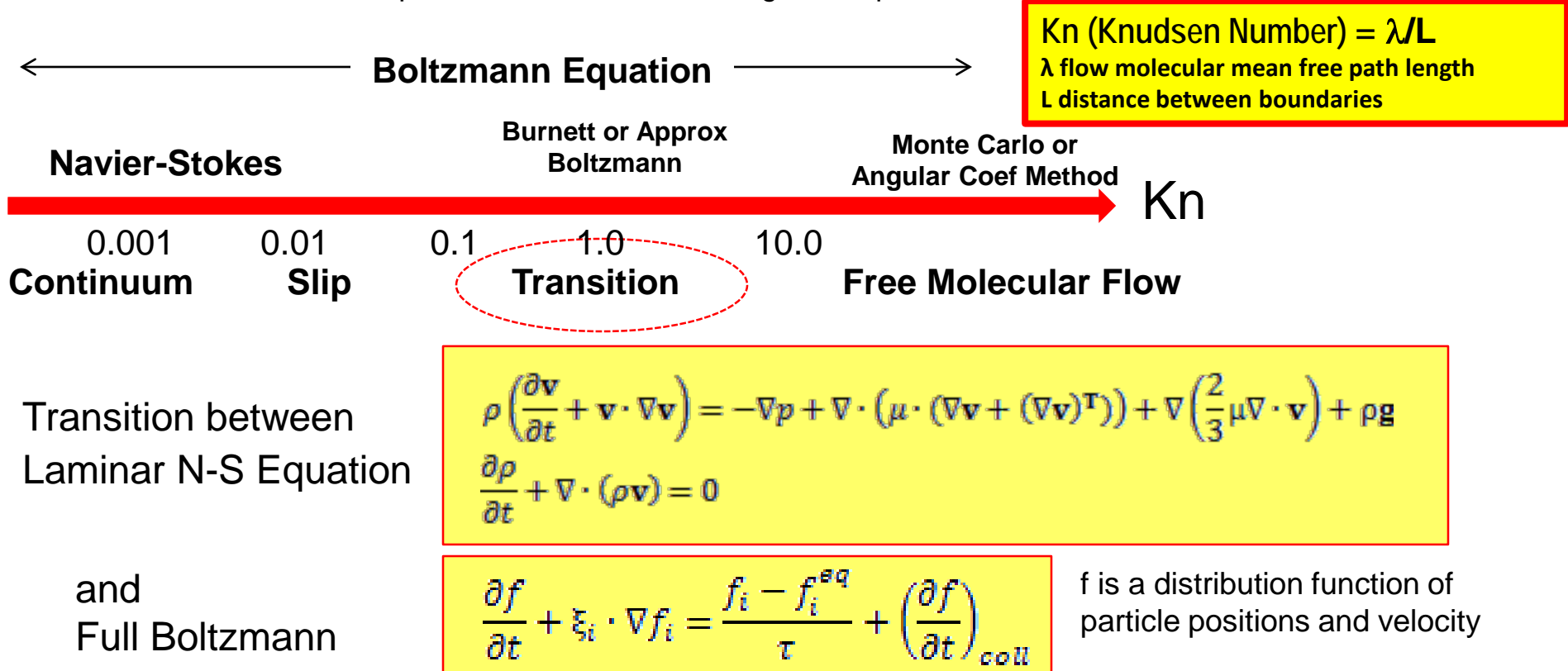


# Knudsen Number and Flow Equations



## ➤ Scale is important to Flow Modeling

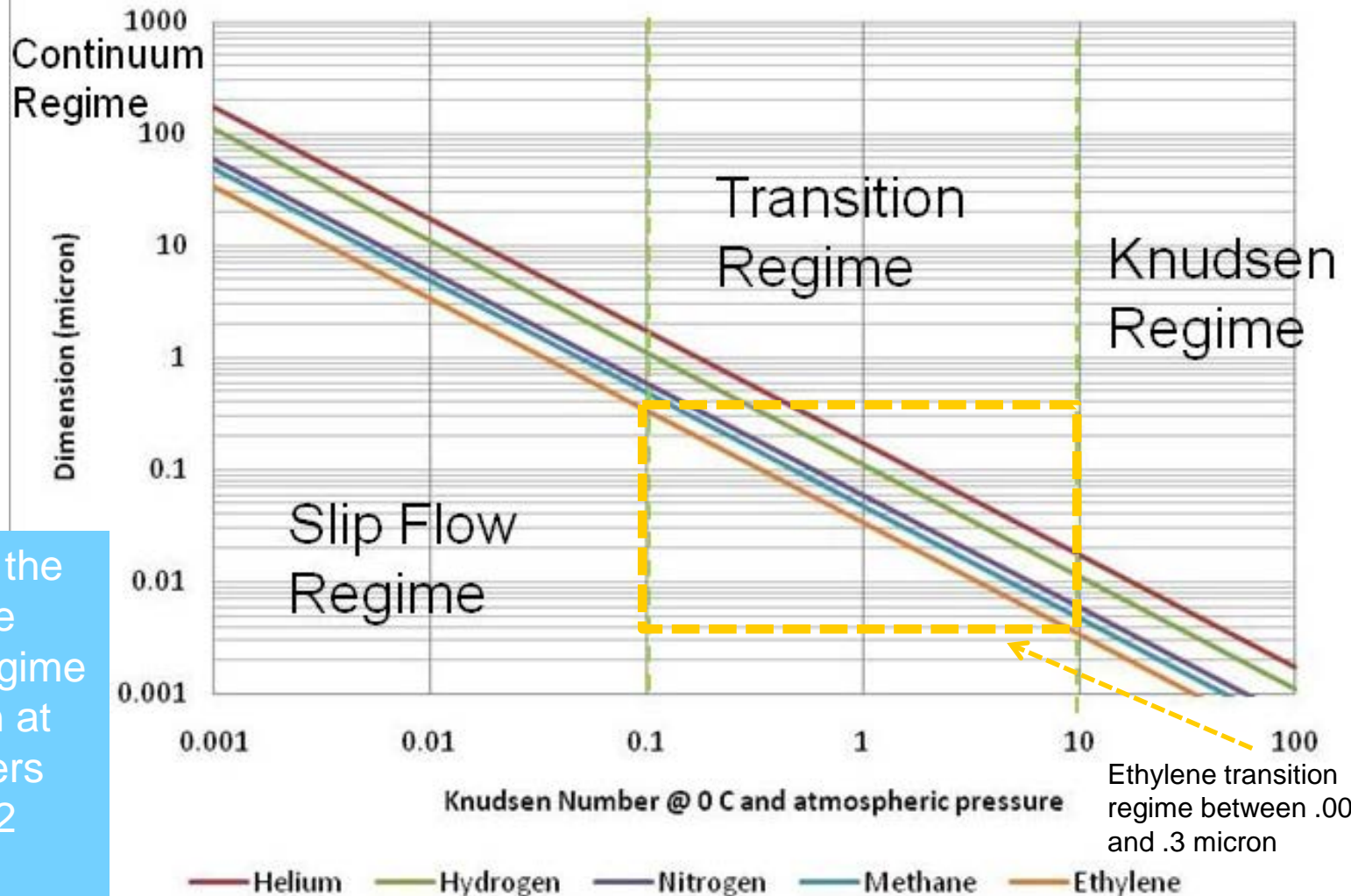
- Continuum Flow is the result of average behavior of huge number of particles
- At smaller scale, there is significant variation from averaging assumptions
- Boltzmann Equation is difficult to solve for large Scale
- Transition Flow regime can use approximations of Boltzmann Equation to solve
- Knudsen Number provides indication of range of Equation validations



# Transition Regime



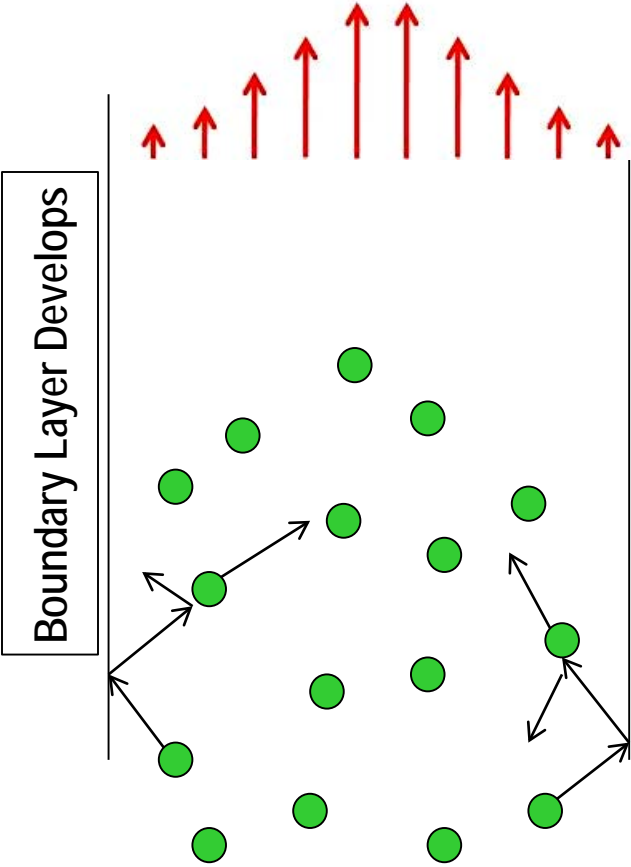
### Length Scale for Different Kn



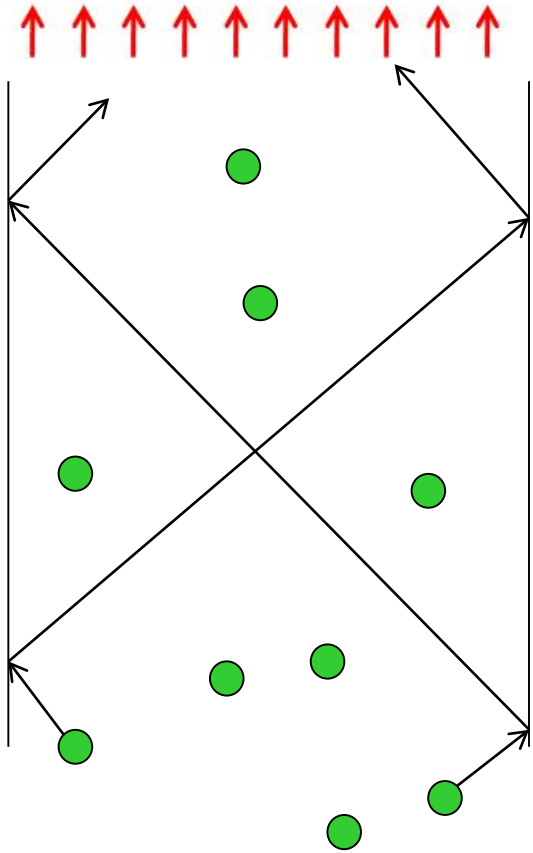
For Helium, the effects of the transition regime can be seen at wall diameters as large as 2 microns

Ethylene transition regime between .003 and .3 micron

# Momentum Transfer



In **continuum regime**, the momentum reflected off the wall is transferred towards the center of the fluid by molecular collisions and reducing the forward momentum near the wall resulting in a parabolic forward momentum distribution



In **Knudsen regime**, the momentum reflected off the wall is transferred to the other wall keeping the forward momentum uniform across the channel diameter

For perfectly reflecting wall, velocity at wall is the amount of velocity change which can be moved to the wall in the mean free path distance  $\lambda \partial v / \partial n$

# Slip Flow through Channel



Assuming narrow gap through parallel plates, perfect gas, dynamic viscosity is pressure independent

$$Q_m = \frac{\Delta P P_m w b^3}{12 \mu R T L} (1 + 6 A_1 K_n)$$

Wall boundary condition

$$v = A_1 \lambda \frac{\partial v}{\partial n}$$

where  $\frac{\partial v}{\partial n}$  is the derivative of velocity normal to boundary,

$$A_1 = \frac{2 - \sigma}{\sigma}, \text{ and } \sigma \text{ diffusive reflection fraction}$$

Slip factor can be used to indicate the increase of the flow against nonslip flow

$$S = 1 + 6 A_1 K_n$$

where  $Q_m$  volumetric flow rate at outlet

$\Delta P$  = Difference between Outlet and Inlet Press

$P_m$  = Average of Outlet and Inlet Press

$w$  = channel width

$b$  = channel gap (height)

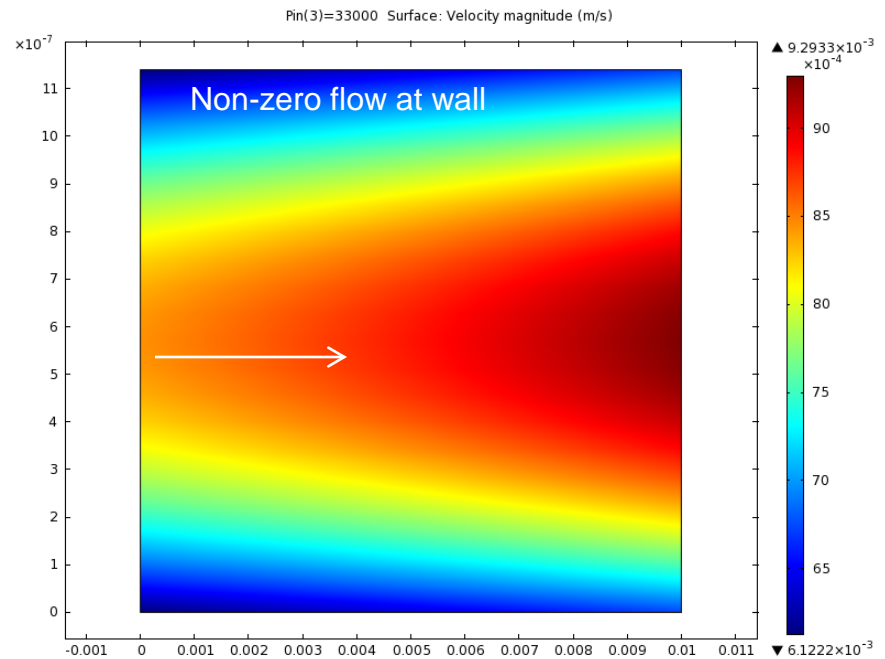
$\mu$  = dynamic viscosity

$R$  = gas constant

$T$  = Absolute Temperature

$L$  = Length of channel

$A_1$  = Reflectivity Factor (typically between 1 to 1.4 )



# Approaches to Transition Flow

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Transition Flow is still an area of active research

## ➤ Higher Order Slip Flow

- Boundary Condition  $v = A_1\lambda \frac{\partial v}{\partial n} + A_2\lambda^2 \frac{\partial^2 v}{\partial n^2}$

## ➤ Diffusion Modified Navier Stokes Equation

- Introduces a self diffusion term  $\frac{\partial \rho}{\partial t} + \nabla \cdot (\rho \mathbf{v}) = -\nabla \cdot \mathbf{j}^D$

## ➤ Burnett Equation

- Approximate Boltzmann Equation to 2<sup>nd</sup> order in Kn

## ➤ Molecular Dynamics

## ➤ Direct Simulation Monte-Carlo

## ➤ Boltzmann BGK

- COMSOL method – Simplifies Collision Operator term  $\left(\frac{\partial f}{\partial t}\right)_{coll}$

## ➤ Dusty Gas

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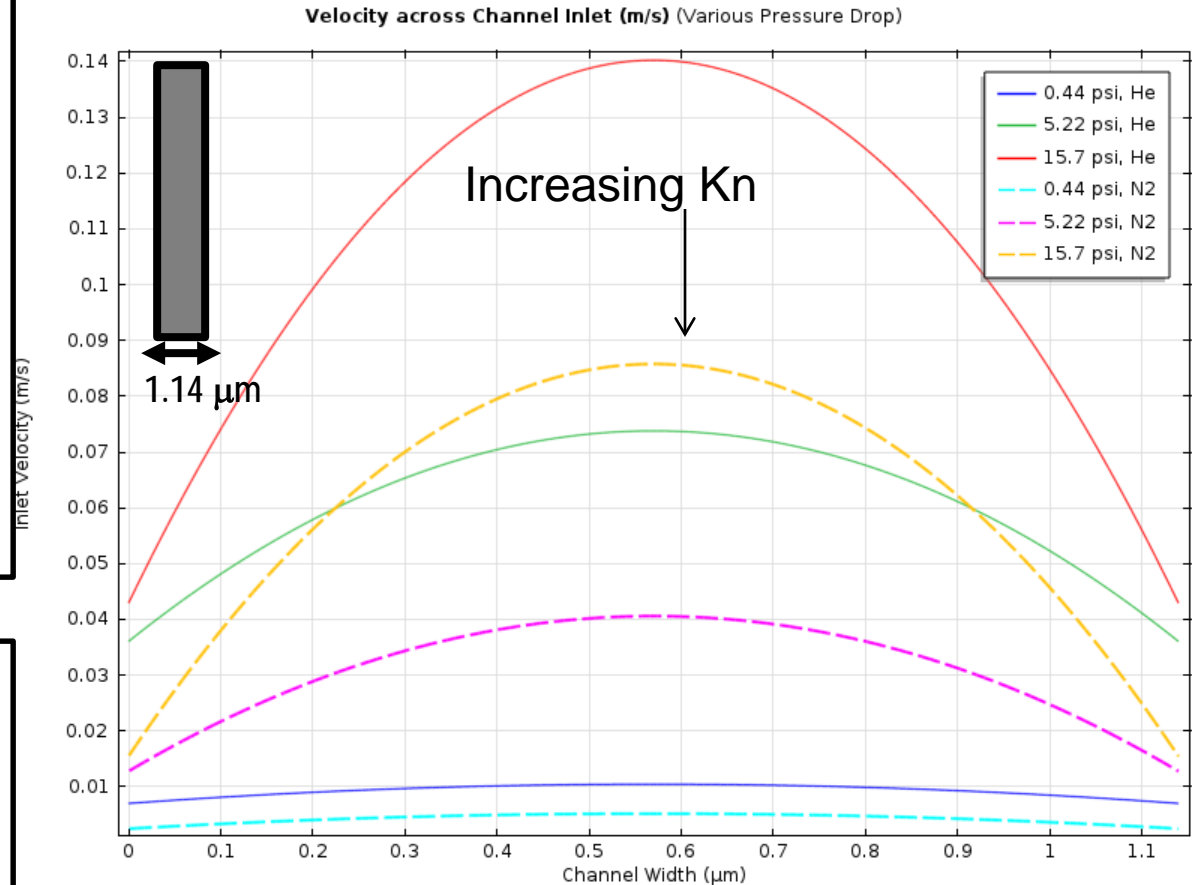


# 2<sup>nd</sup> Slip: Impact of Pressure on Pure Gases



As the average pressure goes down, the Knudsen number goes up and molecules are able to recoil further from the walls. This results in less drag on the wall, so the velocity profile flattens.

Helium has higher Knudsen number than Nitrogen so for the same conditions it has more slip on the wall



Channel width: 1.14 µm  
Outlet pressure: 4.35 psia

# Local Knudsen Number

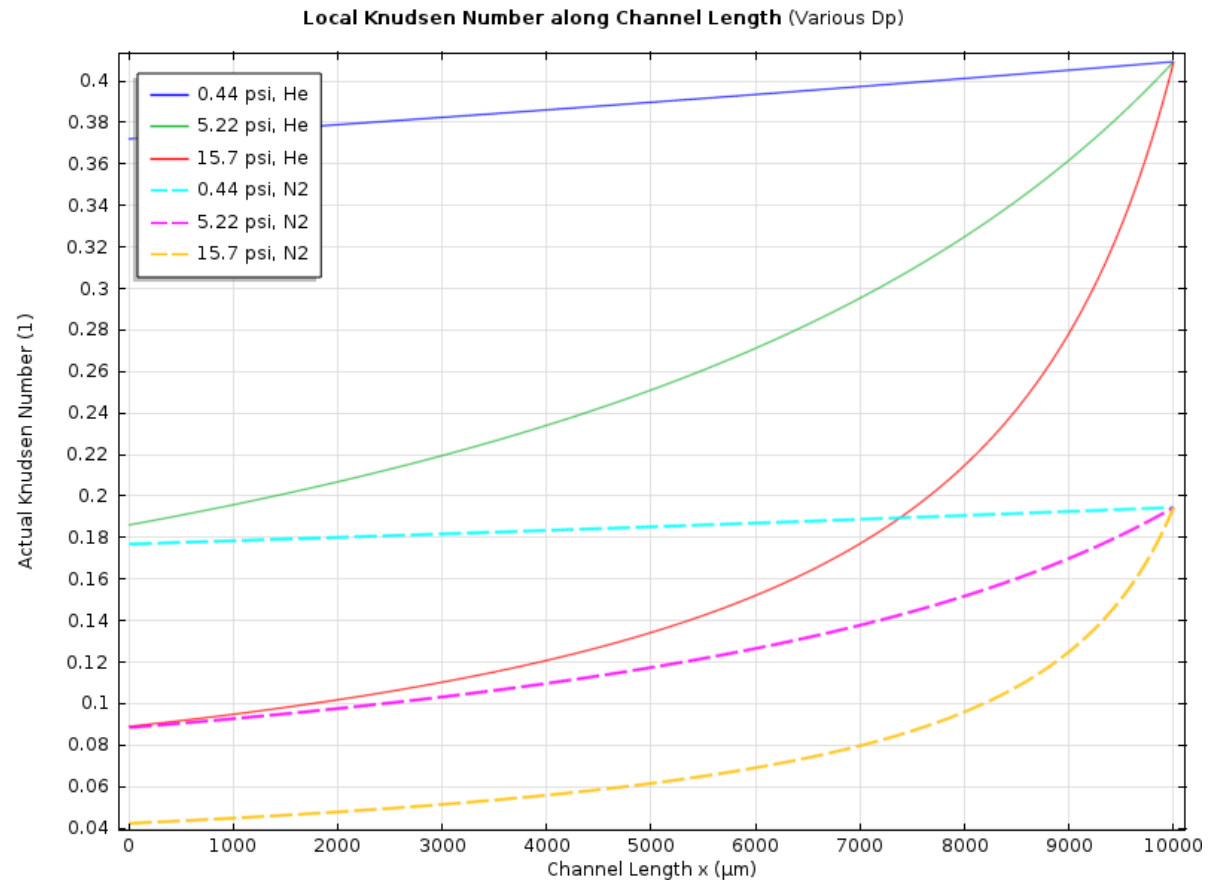


## ➤ Knudsen Number is Pressure Dependent

- Knudsen Number at Average Pressure is Often Used
- Amount of Slip at the Wall depends on the local Pressure

Local Knudsen number varies inversely with the Local Pressure

The greater the pressure drop, the greater the variation of the Slip



# Slip Order and Slip Coefficient



➤ 2<sup>nd</sup> Order Slip factor increases for larger Knudsen #

$$S \approx 1 + 6 A_1 K_n + 12 A_2 K_n^2 *$$

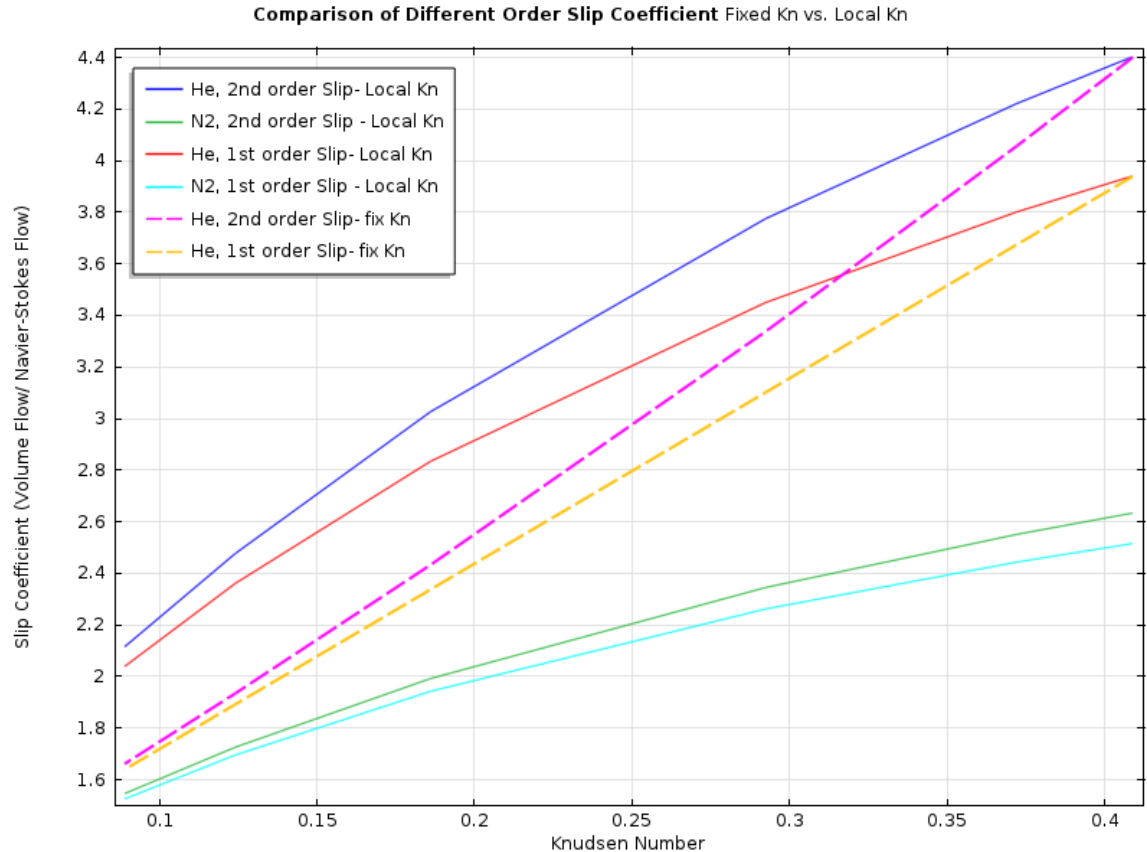
Nitrogen  $A_1 = 1.3, A_2 = 0.26$

Helium  $A_1 = 1.2, A_2 = 0.23$

$A_1$  determined by molecular spectroscopy techniques for glass and silicon

$A_2$  determined by fitting data

The Slip Coefficient is significantly increased when the Local Kn (instead of the Kn at average pressure) is used to solve for Flow



Channel width: 1.14  $\mu\text{m}$   
 Outlet pressure: 4.35 psia

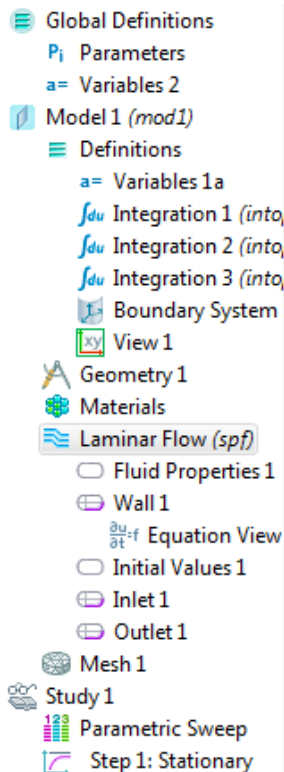
\*Maurer, J., Tabeling, P., Joseph, P. & Willaime, H. "Second-order slip laws in microchannels for helium and nitrogen" *Physics of Fluids* **15**, 2613-2621 (2003).

# Second Order Slip in COMSOL



## ➤ Input 2<sup>nd</sup> Order as moving wall

- Input 1<sup>st</sup> Order with Slip Length
- Need to change discretization to calculate 2<sup>nd</sup> Derivatives
- Flow in x-direction



**Equation**

Equation form: Study controlled

Show equation assuming: Study 1, Stationary

$$\rho(\mathbf{u} \cdot \nabla)\mathbf{u} = \nabla \cdot \left[ -p\mathbf{I} + \mu(\nabla\mathbf{u} + (\nabla\mathbf{u})^T) - \frac{2}{3}\mu(\nabla \cdot \mathbf{u})\mathbf{I} \right] + \mathbf{F}$$
$$\nabla \cdot (\rho\mathbf{u}) = 0$$

**Physical Model**

**Advanced Settings**

**Discretization**

Discretization of fluids: P2 + P1

**Dependent Variables**

**Equation**

Show equation assuming: Study 1, Stationary

$$\mathbf{u} - \mathbf{u}_{w,t} = \frac{L_s}{\mu} \tau_{n,t}$$
$$\mathbf{u}_{w,t} = \mathbf{u}_w - (\mathbf{u}_w \cdot \mathbf{n})\mathbf{n}$$

**Boundary Condition**

Boundary condition: Slip velocity

Velocity of moving wall:

|                |                           |   |     |
|----------------|---------------------------|---|-----|
| $\mathbf{u}_w$ | -A2*mfp <sup>2</sup> *uyy | x | m/s |
|                | 0                         | y |     |

Use viscous slip

Slip length: User defined

$L_s$  mfp<sup>2</sup>\*((2-sigma)/sigma) m

Use thermal creep

**Constraint Settings**

Use weak constraints

# Self Diffusion Model in COMSOL



$$\frac{\partial \rho}{\partial t} + \nabla \cdot (\rho \mathbf{v}) = -\nabla m^D$$

Add as a weak contribution in Laminar flow model

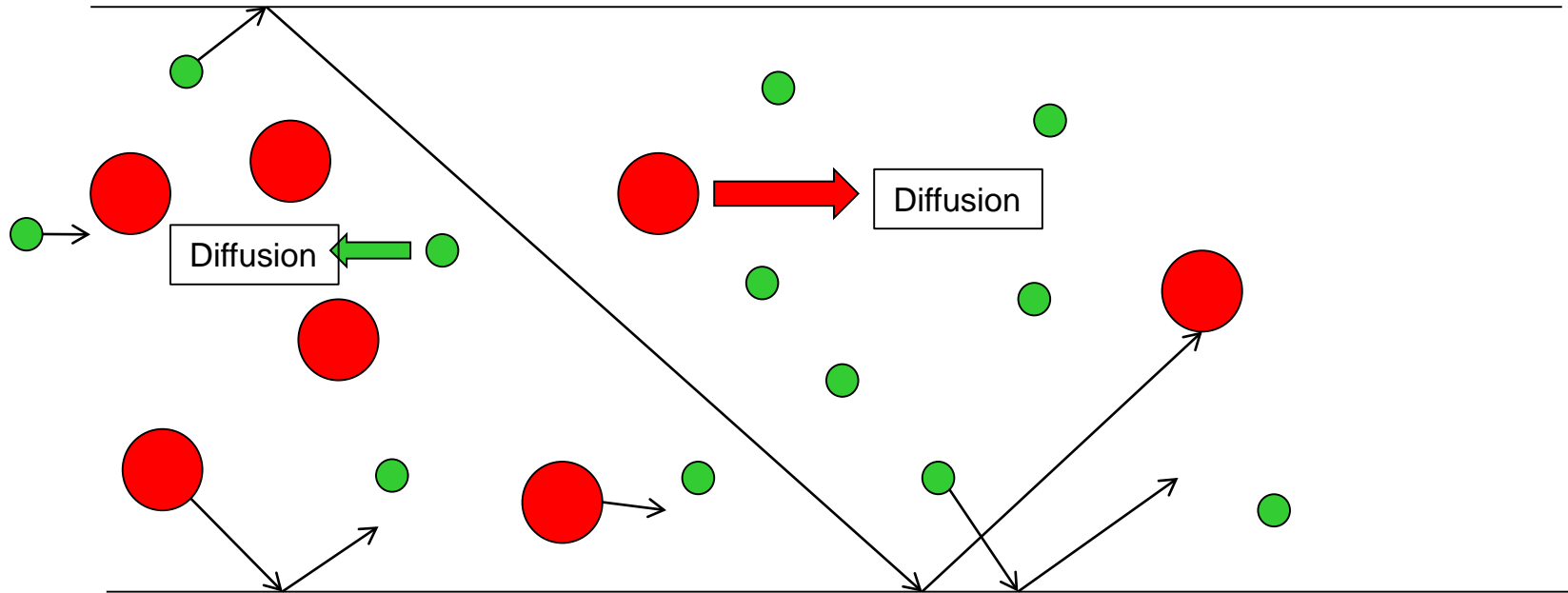
Variables

| Name     | Expression        | Unit                  | Description                  |
|----------|-------------------|-----------------------|------------------------------|
| Df       | spf.mu/spf.rho    | m <sup>2</sup> /s     |                              |
| mdotD1   | -spf.rho*Dfc*px/p | kg/(m <sup>2</sup> s) | Mass transport               |
| tau11    | 4/3*mdotD1*u      | Pa                    | MT diffusive xx term         |
| dtau11x  | d(tau11,x)        | N/m <sup>3</sup>      | derivative of tau11 in x     |
| dmdotD1x | d(mdotD1,x)       | kg/(m <sup>3</sup> s) | derivative of Mass Transport |
| udiff1   | mdotD1/spf.rho    | m/s                   | Diffusion Velocity           |
| utot     | u+udiff1          | m/s                   | Total Velocity               |

Results similar to 2<sup>nd</sup> Order Slip

Need to introduce a volume force

# Dusty Gas: Binary Molecular Flow



The larger particles are more likely to collide with other particles and transfer their momentum to other particles. The momentum transfer from the wall is more likely to be moved towards the center

Molecular diffusion will move the species toward the lower concentration, dragging some of the larger molecules forward and holding some of the smaller molecules back

# Binary Flow through Pore



## Dusty Gas Model

Flux of species "a" is given by

$$N_a = -D_a \nabla c - \frac{x_a D_a}{D_{ab}} \left( \frac{D_a \nabla c_a + D_b \nabla c_b}{x_a \gamma_a + x_b \gamma_b} \right) + x_a N^v.$$

The equation is annotated with arrows pointing to its components:

- Knudsen Diffusion**: points to the term  $-D_a \nabla c$ .
- Fickian Diffusion**: points to the term  $D_a \nabla c_a$  inside the fraction.
- Binary Diffusion**: points to the term  $D_b \nabla c_b$  inside the fraction.
- Molecular Diffusion**: points to the entire fraction term  $\frac{x_a D_a}{D_{ab}} \left( \frac{D_a \nabla c_a + D_b \nabla c_b}{x_a \gamma_a + x_b \gamma_b} \right)$ .
- Viscous Flux**: points to the term  $+ x_a N^v$ .

where  $c$  is the molar density of the gas mixture, the subscript  $a$  and  $b$  indicates the restrict to the particular species,  $x$  is the fraction,  $D$  is a diffusion coefficient, and  $\gamma$  are ratio of diffusion coefficients.

Fickian Diffusion is partial pressure driven

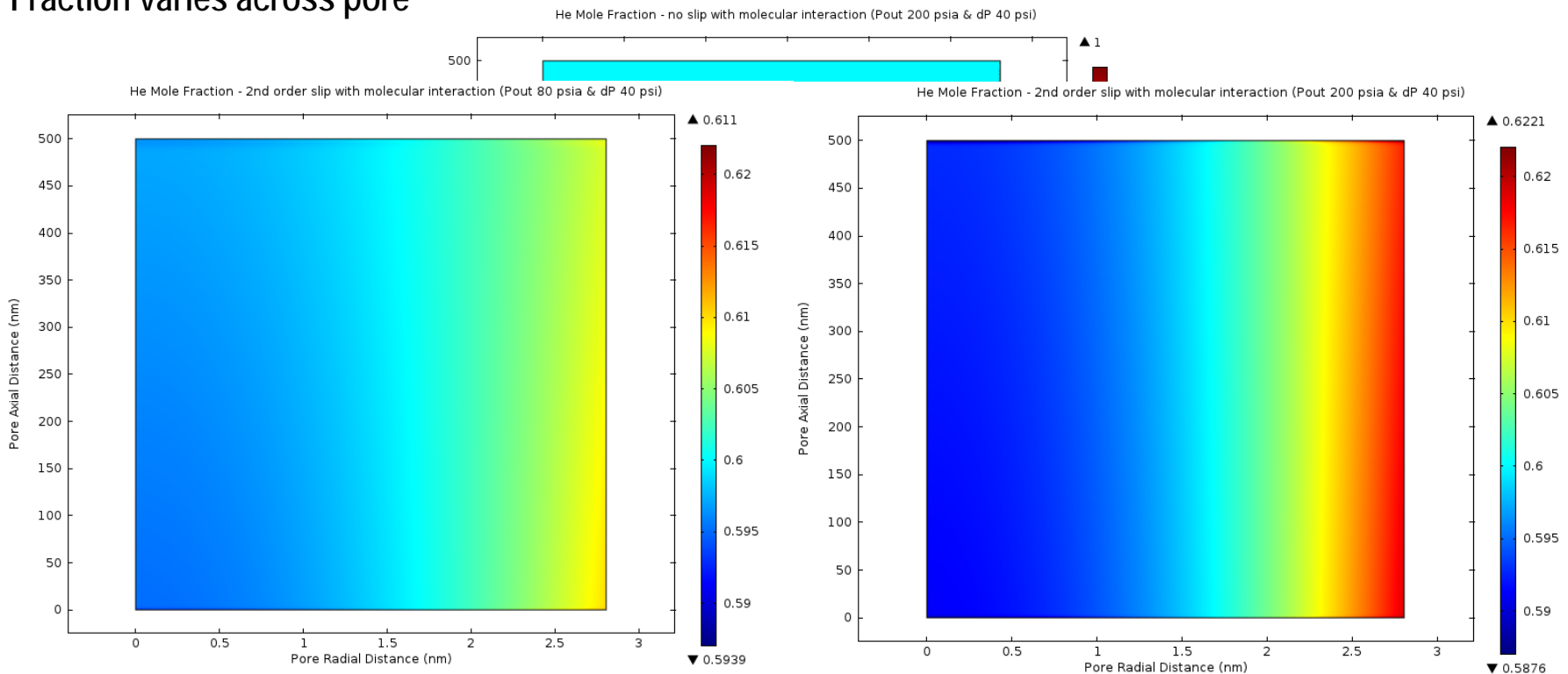
Knudsen Diffusion adds a total pressure component

# Modeling Binary Flow Model



- Each species separately modeled with their own CFD physics using the same mixture viscosity, but the gas densities are based on the individual molecular weight and the slip constants depend on the species.
- Flow of the gas mixture is weighted average of the flow of these individual components.
- Mole fraction approximated from relative velocity changes for each species ( a PDE model of the mole fraction can be included for molecular diffusion effects)

With Slip Conditions, Mole Fraction varies across pore





# Impact of Binary Mixture on Knudsen Number



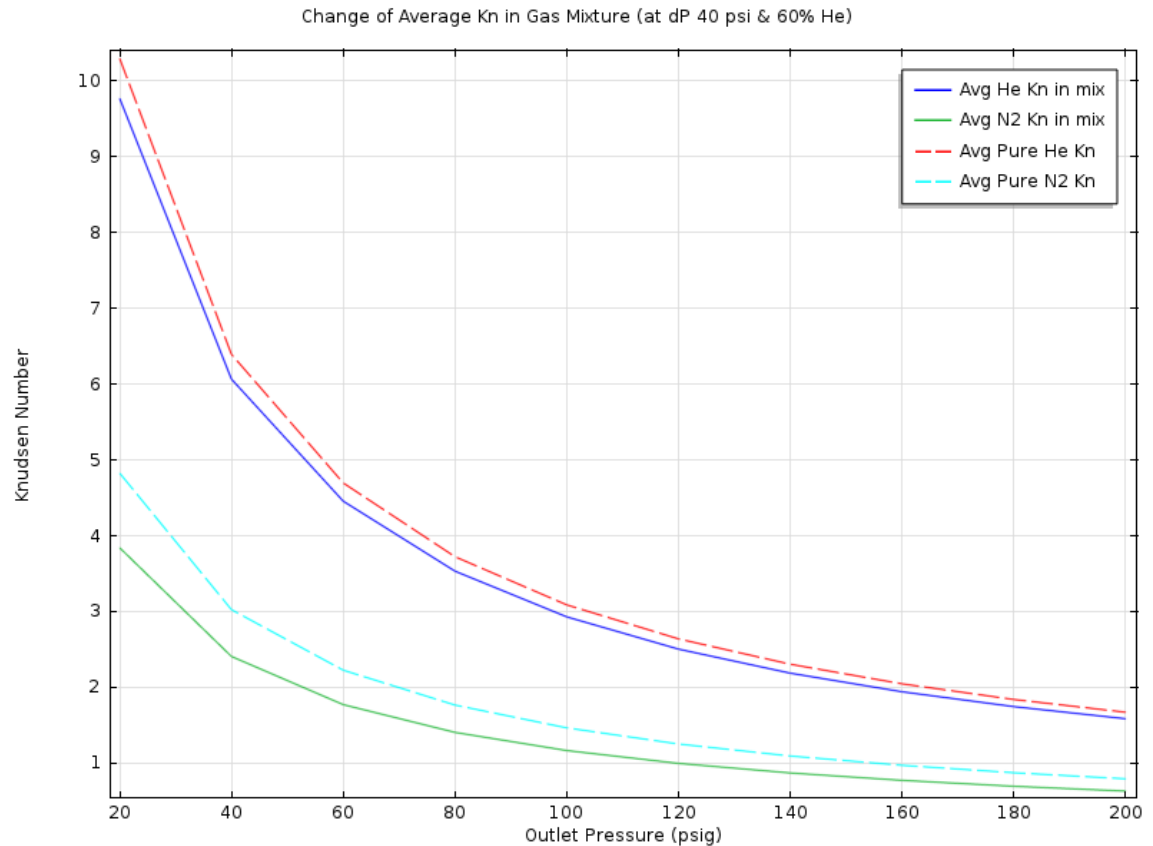
## Mean Free Path of Gas Component in Mixture

For a molecule in a binary gas mixture, the mean free path is given by

$$\lambda_1 = \frac{1}{n_1 \pi \sigma_{11}^2 \sqrt{2} + n_2 \pi \sigma_{12}^2 \sqrt{1 + m_1/m_2}}$$

where  $n_i$  is the number density,  $\sigma_{ij}$  is the collision diameter, and  $m_i$  is the molecular weight.

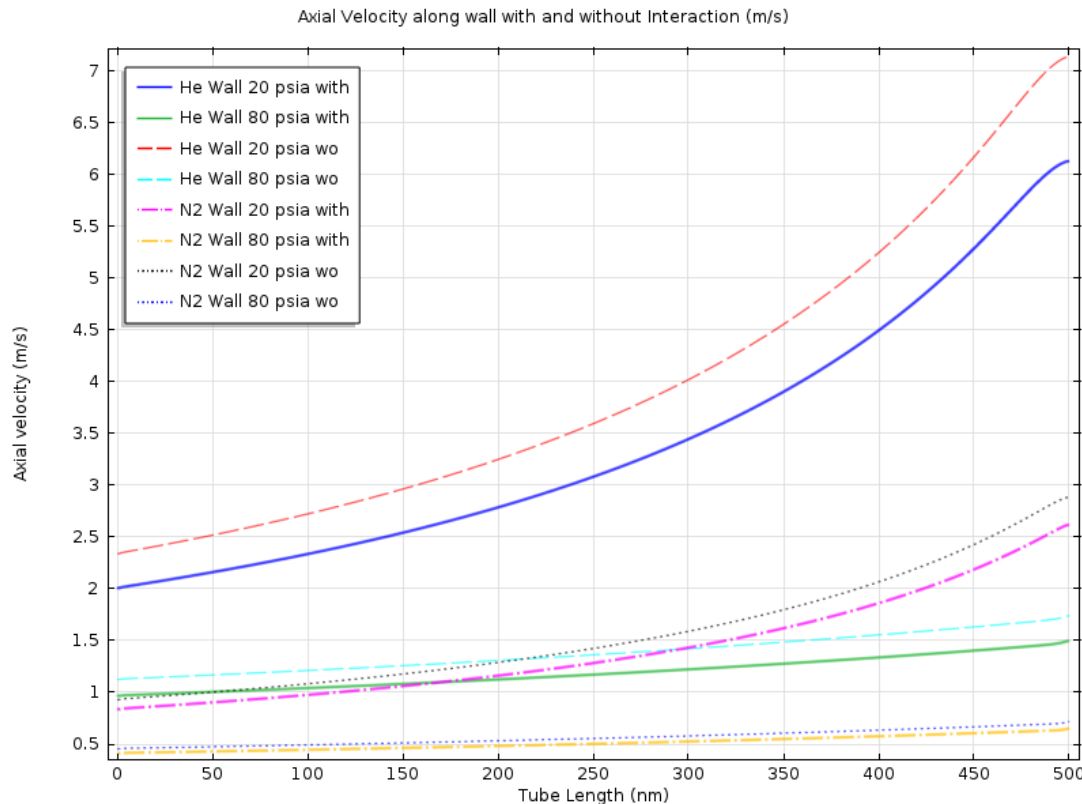
In the Binary Mixture, the mean free path used in the wall boundary condition needs to be modified for the species interactions



# Impact of Molecular Interaction on Velocity



- The molecular interactions reduces the velocity of each species through the pore
  - Impacted by change in mean free path
- Higher Knudsen have higher speeds
  - Molecular interaction has greater impact for higher Knudsen Number
- Permeance of Gas Mixture is lower than weighted average permeance of species



5.6 nm pore with 40 psi pressure drop and 60 mole% Helium

# Transition Flow in COMSOL



Based on Boltzmann BGK  
COMSOL method – Simplifies Collision Operator term  $\left(\frac{\partial f}{\partial t}\right)_{coll}$

- Transitional Flow (tran)
  - Flow Properties 1
    - Equation View
    - Wall 1
    - Continuity on Interior Boundary 1
    - Initial Values 1
    - Inlet 1
    - Outlet 1
    - Equation View
- Transitional Flow 2 (tran2)
  - Flow Properties 1
    - Wall 1
    - Continuity on Interior Boundary 1
    - Initial Values 1
    - Reservoir 1
    - Reservoir 2
    - Equation View
- Laminar Flow 2Slip (spf2)
  - Fluid Properties 1
  - Initial Values 1
  - Wall 1
  - Inlet 1
  - Outlet 1
  - Equation View
- Transitional Flow (tran)
  - Flow Properties 1
    - Equation View
    - Wall 1
    - Continuity on Interior Boundary 1
    - Initial Values 1
    - Inlet 1
    - Outlet 1
    - Equation View
- Transitional Flow 2 (tran2)
  - Flow Properties 1
    - Wall 1
    - Continuity on Interior Boundary 1
    - Initial Values 1
    - Reservoir 1
    - Reservoir 2
    - Equation View
- Laminar Flow 2Slip (spf2)
  - Fluid Properties 1
  - Initial Values 1
  - Wall 1
  - Inlet 1
  - Outlet 1
  - Equation View
- Mesh 1
  - Size
  - Free Triangular 1
- Study 1
  - Step 1: Stationary

Active

Override and Contribution

Equation

Show equation assuming:

Study 1, Stationary

$$\xi_i \nabla f_i = \frac{f_i - f_i^{eq}}{\tau}$$

$$N = \sum_i f_i, \quad \rho = \sum_i \frac{M_n f_i}{N_A}, \quad \mathbf{u} = \frac{M_n}{N_A \rho} \sum_i f_i \xi_i$$

$$N_{eq} = N, \quad \mathbf{u}_{eq} = \mathbf{u}$$

$$\tau = \frac{\mu}{\rho c_s^2}, \quad c_s = \sqrt{RT/M_w}, \quad \lambda = \frac{\sum_i w_i \tau |\xi_i f_i}{\sum_i w_i f_i}$$

Specify boundary Conditions in Different way

Active

Override and Contribution

Equation

Show equation assuming:

Study 1, Stationary

$$f_i = \frac{J \cdot f_i^{eq}}{\sum_{(\xi_i - \mathbf{u}_{eq}) \cdot \mathbf{n} > 0} (-\xi_i - \mathbf{u}_{eq}) \cdot \mathbf{n}} f_i^{eq}, \quad (\xi_i - \mathbf{u}_{eq}) \cdot \mathbf{n} < 0$$

$$G = \sum_{(\xi_i - \mathbf{u}_{eq}) \cdot \mathbf{n} > 0} ((\xi_i - \mathbf{u}_{eq}) \cdot \mathbf{n}) f_i$$

$$\xi_i$$

$$\mathbf{u}_{eq} = \mathbf{u}$$

$$J = J(p_0)$$

Boundary condition:

Pressure

Pressure:

$p_0$  p0+dp

- Transitional Flow (tran)
  - Flow Properties 1
    - Equation View
    - Wall 1
    - Continuity on Interior Boundary 1
    - Initial Values 1
    - Reservoir 1
    - Reservoir 2
    - Equation View
- Transitional Flow 2 (tran2)
  - Flow Properties 1
    - Wall 1
    - Continuity on Interior Boundary 1
    - Initial Values 1
    - Reservoir 1
    - Reservoir 2
    - Equation View
- Laminar Flow 2Slip (spf2)
  - Fluid Properties 1
  - Initial Values 1

Show equation assuming:

Study 1, Stationary

$$f_i = \frac{J \cdot f_i^{eq}}{\sum_{(\xi_i - \mathbf{u}_{eq}) \cdot \mathbf{n} > 0} (-\xi_i - \mathbf{u}_{eq}) \cdot \mathbf{n}} f_i^{eq}, \quad (\xi_i - \mathbf{u}_{eq}) \cdot \mathbf{n} < 0$$

$$G = \sum_{(\xi_i - \mathbf{u}_{eq}) \cdot \mathbf{n} > 0} ((\xi_i - \mathbf{u}_{eq}) \cdot \mathbf{n}) f_i$$

$$\xi_i$$

$$\mathbf{u}_{eq} = 0$$

$$J = \left(\frac{1}{2\pi M_w RT}\right)^2 p_0$$

Reservoir

Boundary condition:

Reservoir pressure

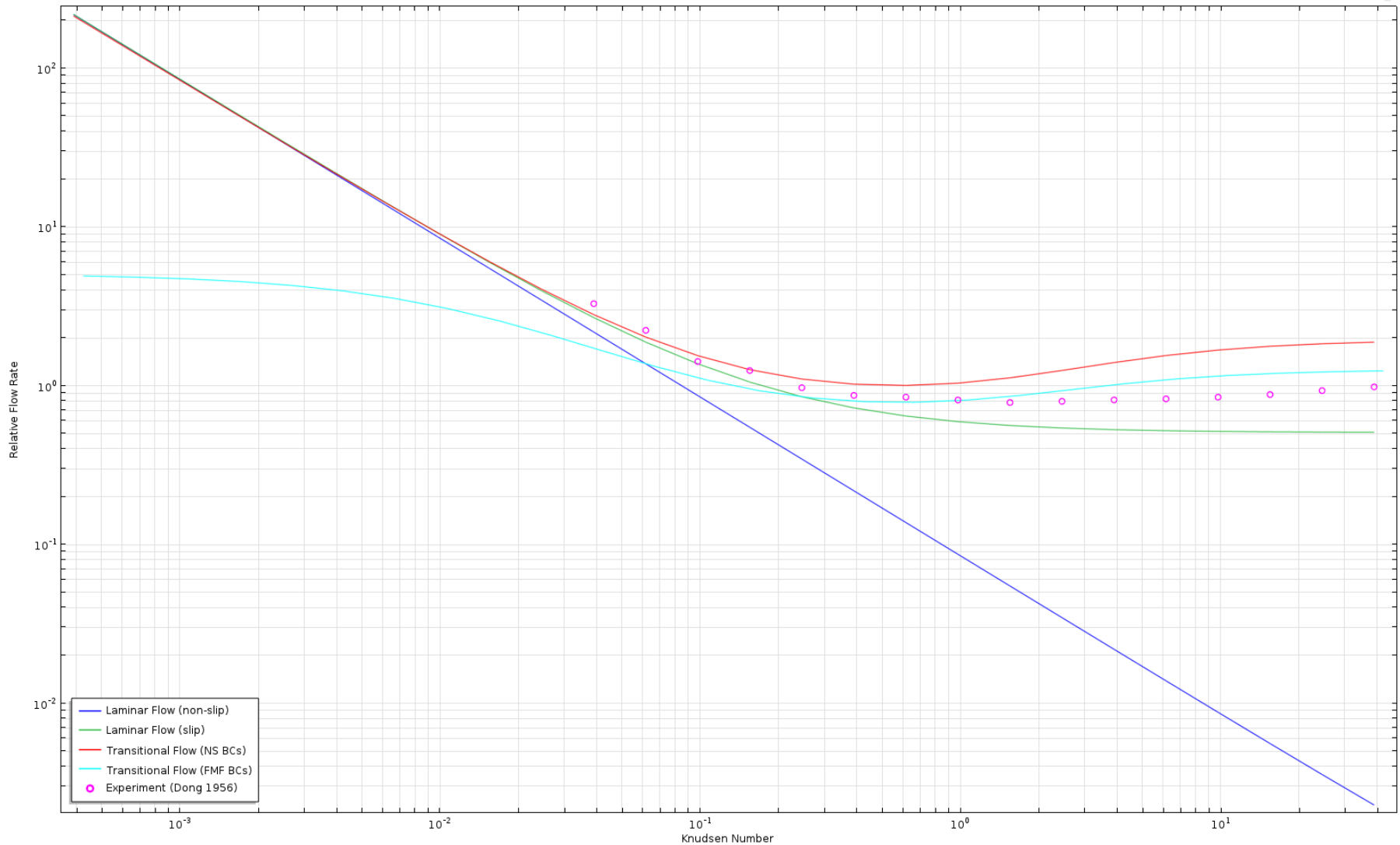
Reservoir pressure:

$p_0$  p0+dp

# COMSOL models in the Transition Regime



Global Global: Transitional Flow (FMF BCs) (1) Global: Experiment (Dong 1956)



From COMSOL's Knudsen\_Minimum Example

# Summary and Conclusions

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- Transition flow Modeling can be done in Multiple Ways
  - Extension of Navier-Stokes (2<sup>nd</sup> Order Slip, Self Diffusion ... )
  - Approximation of Boltzmann Equation
- Developed multi-physics model to understand influence of slip coefficient on single component flow
  - Comparison of 1st and 2nd Order Slip
  - Investigated the influence of pressure on local Kn
  - Investigated the relation between slip order and slip coefficient for helium and nitrogen flow
  - Implementing in COMSOL
- Binary flow modeling
  - Coupled the flow models of the individual species to get binary flow
  - Composition varies in pore with slip
  - Molecular interaction reduces velocity compared to individual species

# Thanks to my Dow Collaborators

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## ➤ Kishori Deshpande

- Alexia Finotello
- John Pendergast Jr
- Mark Brayden



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# Back Up Slides

- Holt, J.K., Park, H.G., Wang, Y., Stadermann, M., Artyukhin, A.B., Grigoropoulos, C.P., Noy, A. & Bakajin, O. "Fast Mass Transport Through Sub-2-Nanometer Carbon Nanotubes" *Science* **312**, 1034-1037 (2006).
- Maurer, J., Tabeling, P., Joseph, P. & Willaime, H. "Second-order slip laws in microchannels for helium and nitrogen" *Physics of Fluids* **15**, 2613-2621 (2003).
- Dongari, N. & Agrawal, A. "Modeling of Navier–Stokes equations for high Knudsen number gas flows" *International Journal of Heat and Mass Transfer* **55**, 4352-4358 (2012)
- Agarwal, R.K., Yun, K.-Y. & Balakrishnan, R. "Beyond Navier--Stokes: Burnett equations for flows in the continuum--transition regime" *Physics of Fluids* **13**, 3061-3085 (2001).



# Case Study: Single Component Diffusion



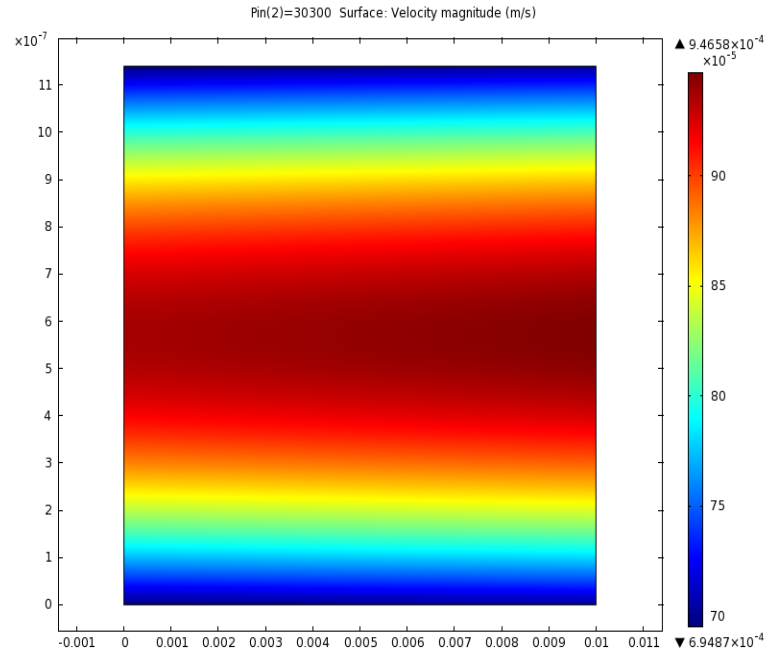
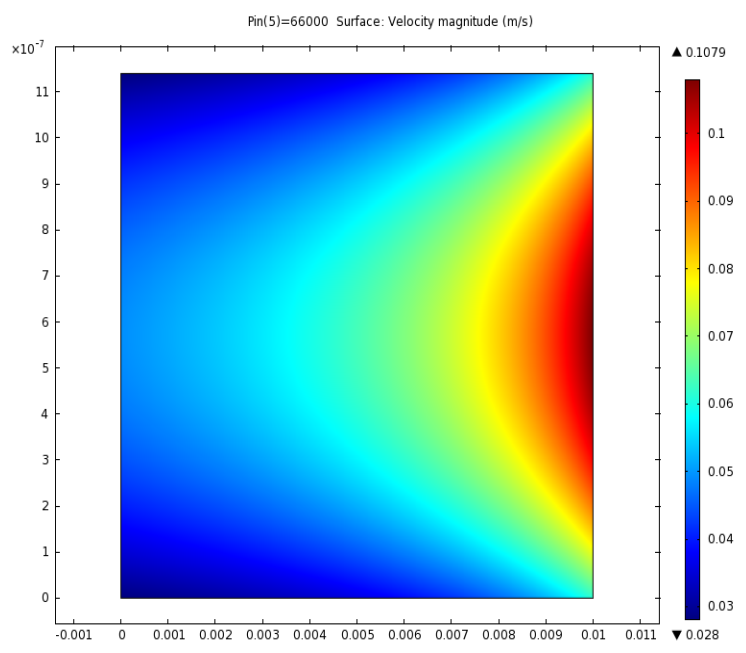
## ➤ Approach

- Laminar Flow Physics in 2 dimensions assuming an infinitely wide channel
- Isothermal conditions, locally fully developed steady flow, and ideal gas behavior
- Maxwell's slip velocity equation

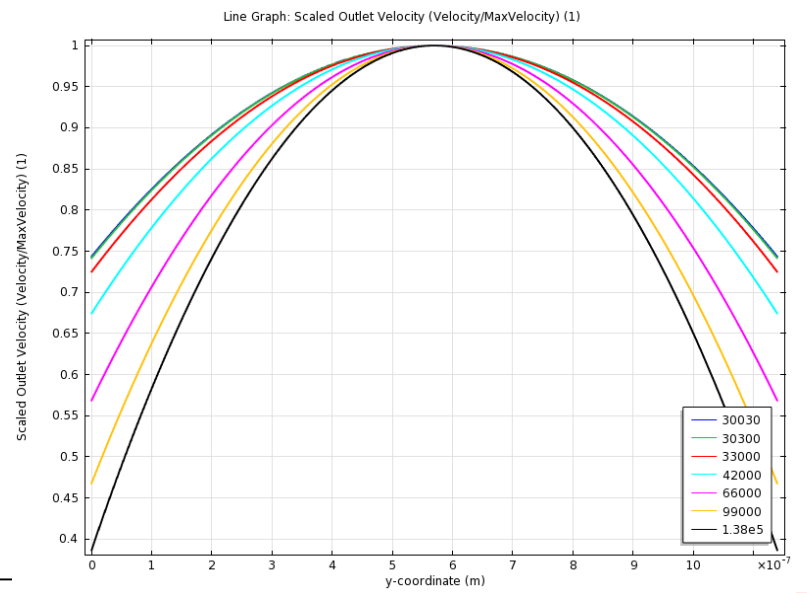
**Parameters**

| Name     | Expression   | Value   | Description                        |
|----------|--|---|------------------------------------|
| hchannel | 1.14[um]   | 1.14E-6 m   | Channel Height                     |
| Lchannel | 10000[um]  | 0.01 m  | Channel Length                     |
| wchannel | 200[um]  | 2.0E-4 m  | Channel Width                      |
| Pin      | .33[bar]   | 33000.0 Pa  | Inlet Pressure                     |
| Pout     | .3[bar]  | 30000.0 Pa  | Outlet Pressure                    |
| Temp     | 293.15[K]  | 293.2 K   | Temperature                        |
| Mn       | 4.0029[g/mol]  | 0.004003 kg/mol   | Molecular Weight                   |
| Mdiam    | 210[pm]  | 2.1E-10 m   | Molecular Diameter                 |
| mfp      | $k_B \cdot \text{Temp} / (\sqrt{2} \cdot \pi \cdot (\text{Mdiam}^2) \cdot (\text{Pin} + \text{Pout}) / 2)$ | 6.558E-7 m  | Mean Free Path                     |
| KnudsenN | mfp/hchannel   | 0.5752  | Knudsen Number                     |
| sigma    | .91  | 0.91  | Wall reflect fraction              |
| A2       | .23  | 0.23  | 2nd order slip coeff               |
| PsqDiff  | $(\text{Pin}^2 - \text{Pout}^2) / 2$   | 9.45E7 kg <sup>2</sup> /(m <sup>2</sup> ·s <sup>4</sup> ) | Average Difference of Press Square |

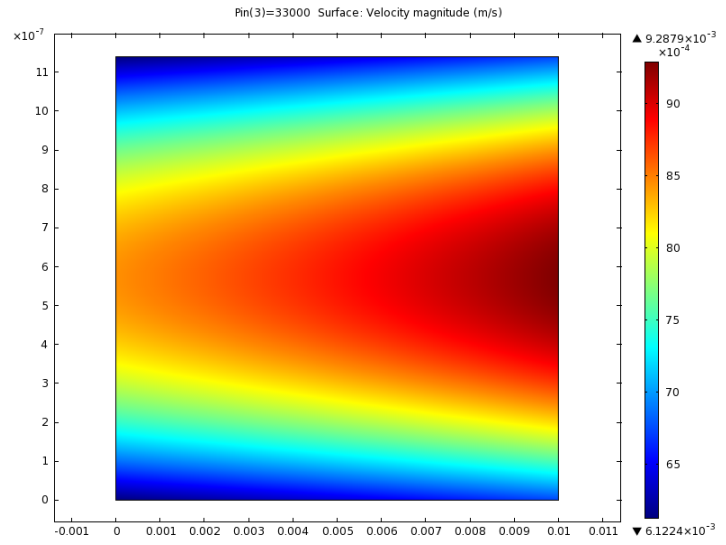
# Single Component Diffusion: 1<sup>st</sup> order Slip



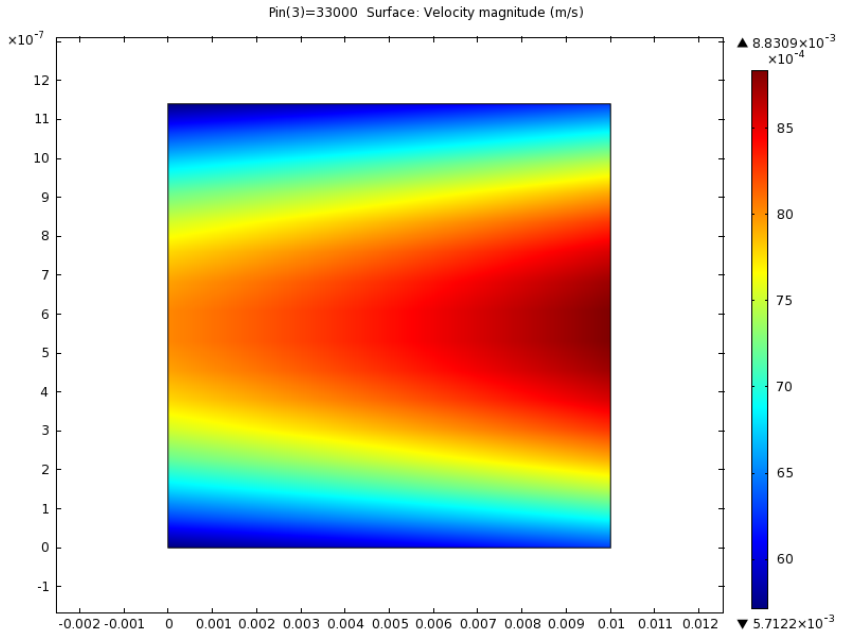
**Velocity Profile with First Order Slip at Pin= .66 bar (L) and =.303 bar (R)**



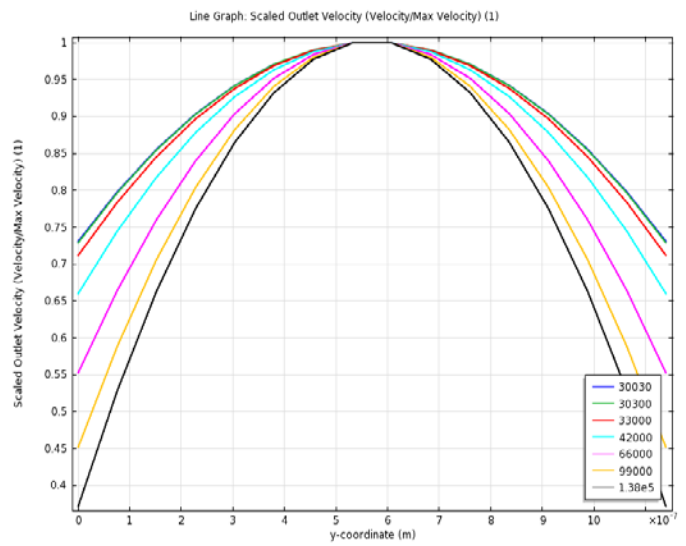
# Single Component Diffusion: 2<sup>nd</sup> order Slip



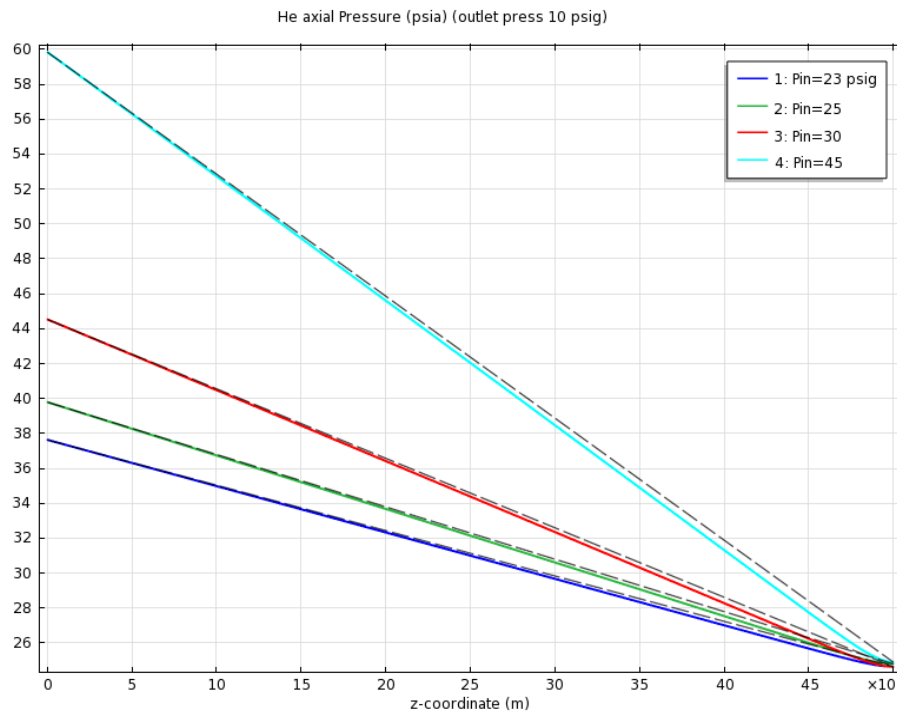
1<sup>st</sup> order Slip



2<sup>nd</sup> order Slip



# Knudsen Number Variation down the Pore



As pressure drops along the length of pore, the Knudsen number changes. For high pressure drop, the flow can range from the slip flow regime to the Knudsen regime

With gas mixture, one component could be in the Knudsen regime while another is still in the transition regime

There are a number of competing models in the literature, so experimentation is critical

