

# Modeling Of Mixing-sensitive Pharmaceutical Drug Substance Production Processes In Batch Reactors

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# Impact of Mixing on Chemical Unit Operations in Pharmaceutical Industry

- ◆ Many chemical unit operations in drug substance production are performed in stirred tank reactors and are transport dependent. Therefore, they can be mixing sensitive.
  - Biphasic reactions
  - Extraction
  - Crystallizations
- ◆ Multiple mixing parameters must be considered during scale-up.
  - Reactor and impeller geometry
  - Shear rate
  - Specific energy dissipation rate
  - Power input per volume



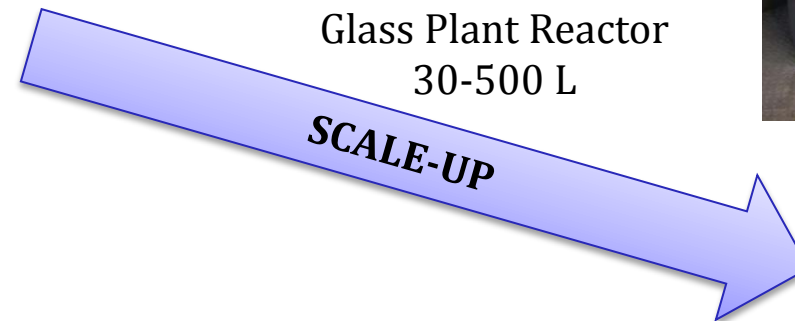
Lab Reactor  
0.1-40 L



Glass Plant Reactor  
30-500 L

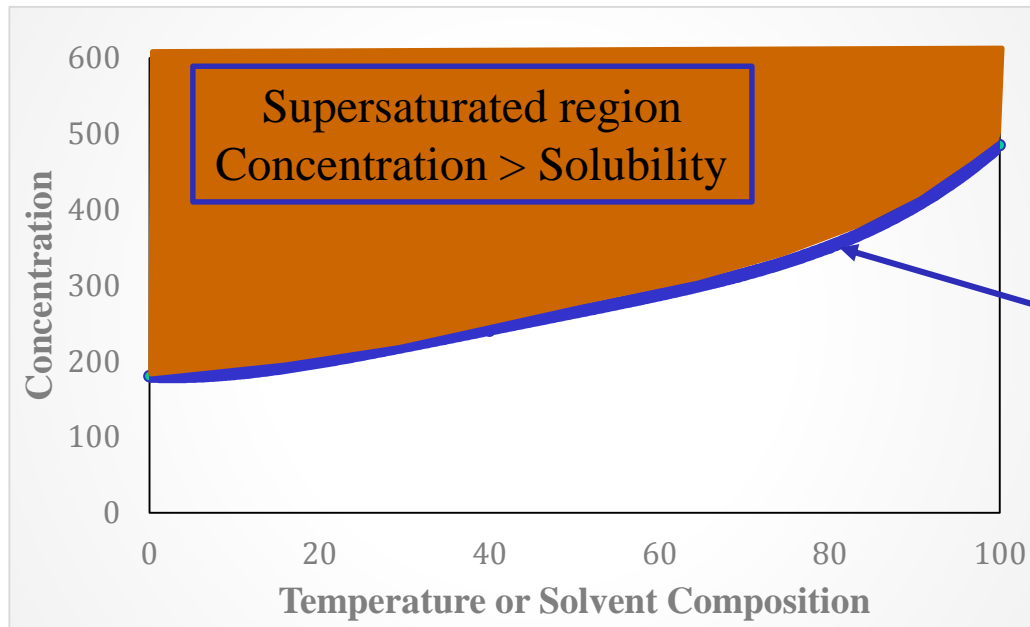


Plant Reactor  
1000- 40000 L



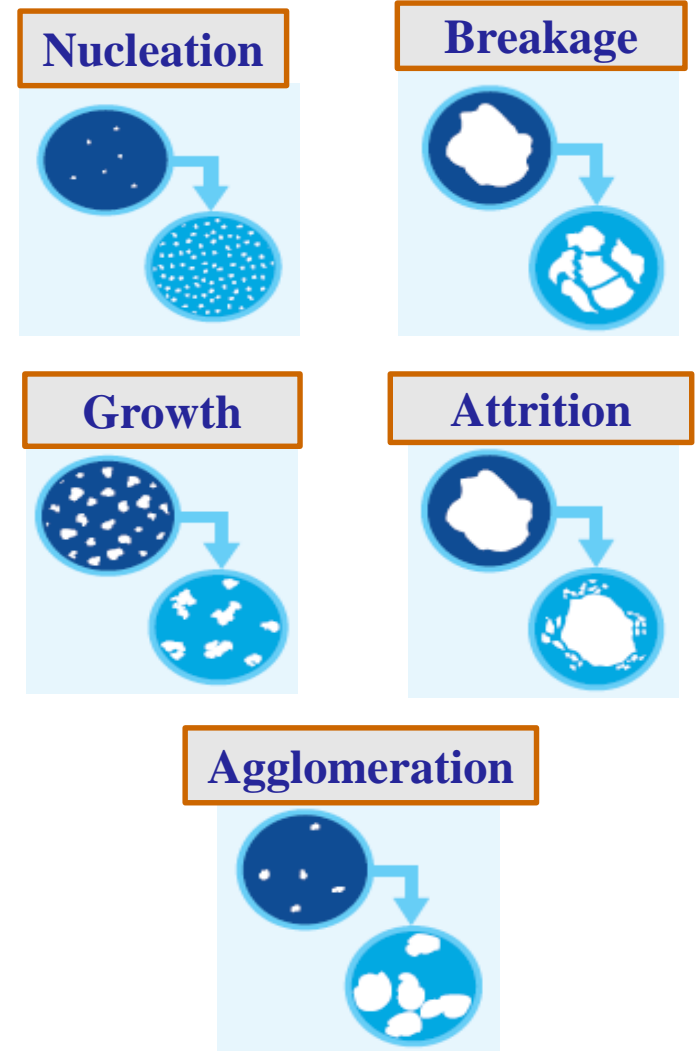
# Case Study: Crystallization

## - Drug Substance Purification Process



### ◆ Typical crystallization process operations:

- Antisolvent\* addition to achieve supersaturation
- Heating to increase nucleation and growth kinetics
- Cooling and aging for the completion of crystallization



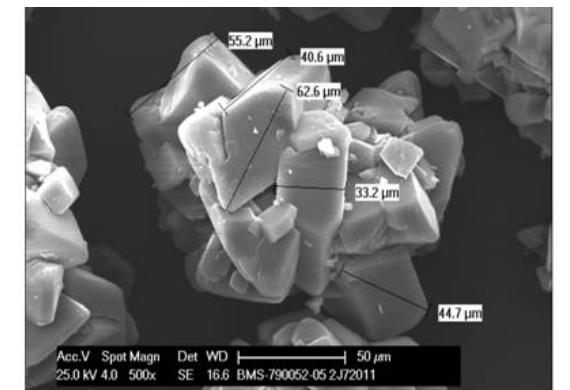
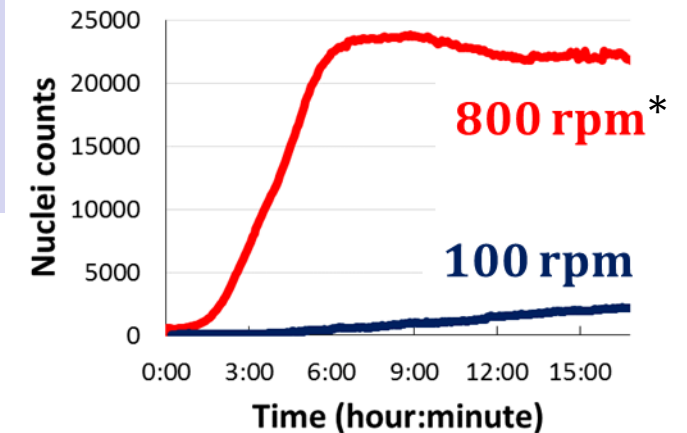
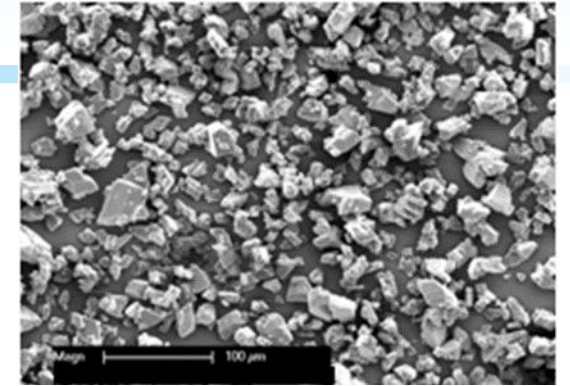
\*antisolvent – solvent with low product solubility

# Mixing Sensitivity in Crystallization

## Potential Consequences

**Fast mixing**

- Fast uncontrolled nucleation
  - Particle attrition
  - De-agglomeration



\*rpm – rotations per minute

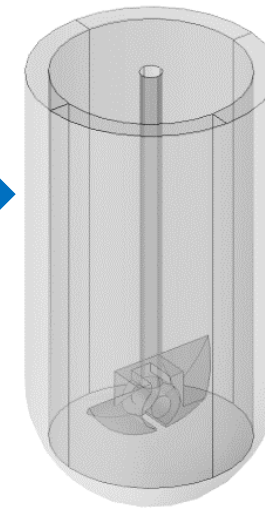
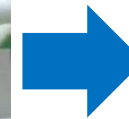
# COMSOL Model to Assess Mixing Sensitivity in Drug Substance Crystallization

- ◆ Solve Navier-Stokes equation on the 3D reactor geometry
  - Rotating Machinery, Turbulent Flow k- $\omega$  model
    - Frozen rotor study – Reynolds-averaged NS
    - Time dependent study
- ◆ Account for specific reactor geometry and configurations
- ◆ Provide solution of the flow field to determine velocity, shear and energy dissipation rate profiles throughout the reactor
- ◆ Provide fast estimation of mixing attributes at scale
- ◆ Couple multiple physics
  - Flow
  - Reactions/transport of species
  - Heat transfer

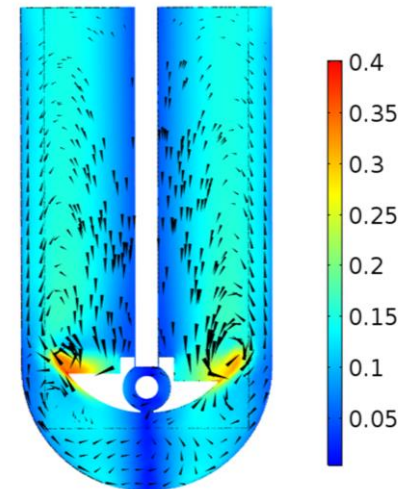
$$\frac{\partial \rho}{\partial t} + \nabla \cdot (\rho \mathbf{u}) = 0, \text{ ----- Continuity Equation (1)}$$

$$\frac{\partial \mathbf{u}}{\partial t} + (\mathbf{u} \cdot \nabla) \mathbf{u} = -\frac{1}{\rho} \nabla p + \mathbf{F} + \frac{\mu}{\rho} \nabla^2 \mathbf{u}, \text{ ----- Equations of Motion (2)}$$

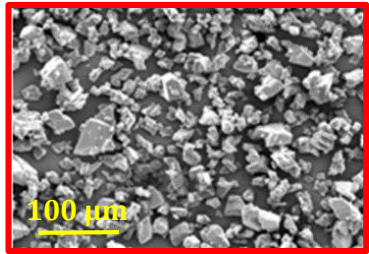
$$\rho \left( \frac{\partial \varepsilon}{\partial t} + \mathbf{u} \cdot \nabla \varepsilon \right) - \nabla \cdot (K_H \nabla T) + p \nabla \cdot \mathbf{u} = 0. \text{ ----- Conservation of Energy (3)}$$



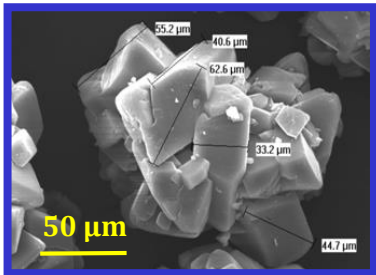
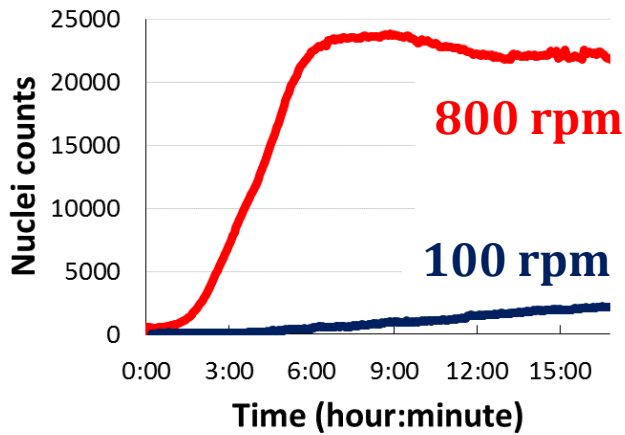
Velocity Profile



# Mixing Attributes for Fast and Slow Mixing in Lab Reactor

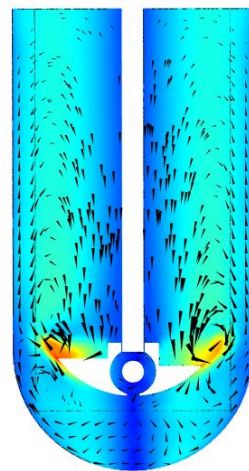
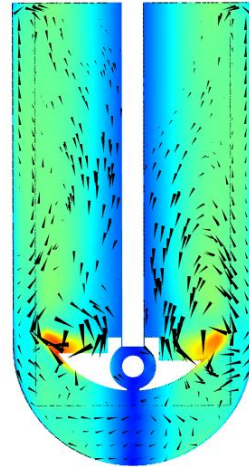


- Fast nucleation
- Small particle size

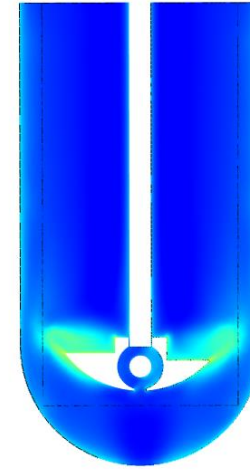
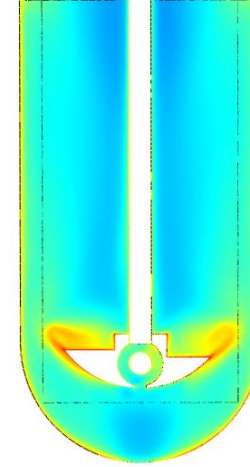


- Slow nucleation
- Agglomeration
- Large particle size

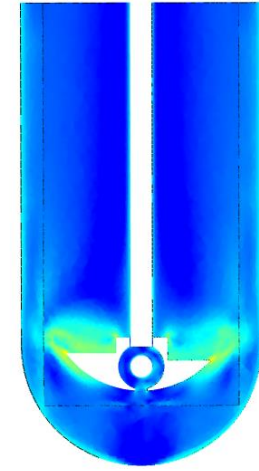
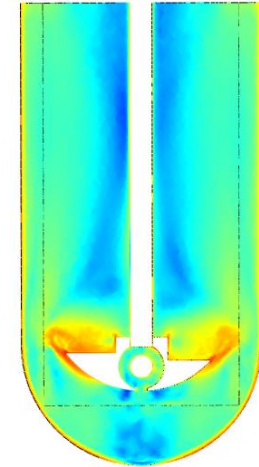
Velocity (m/s)



Specific energy dissipation rate\* (1/s)



Shear rate (1/s)

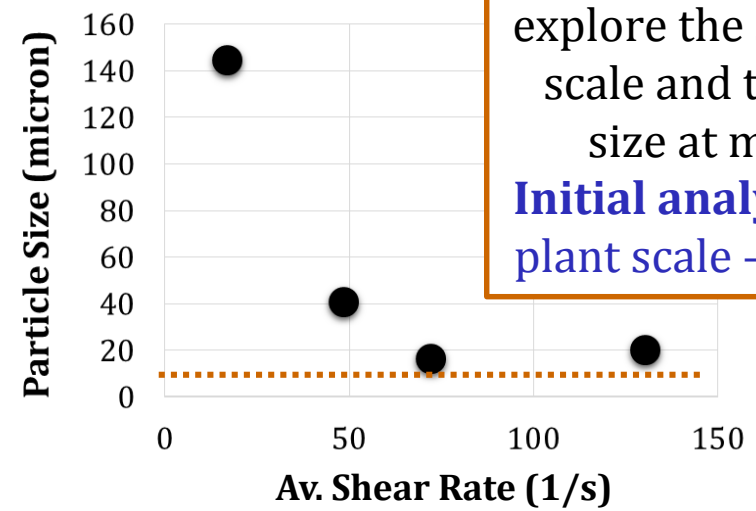
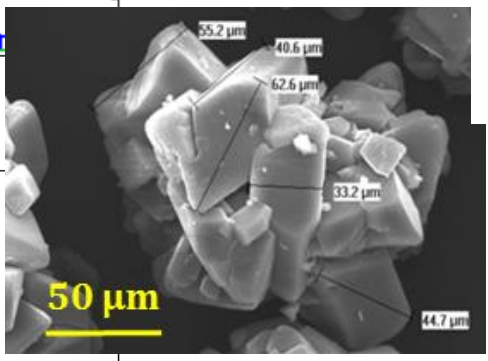
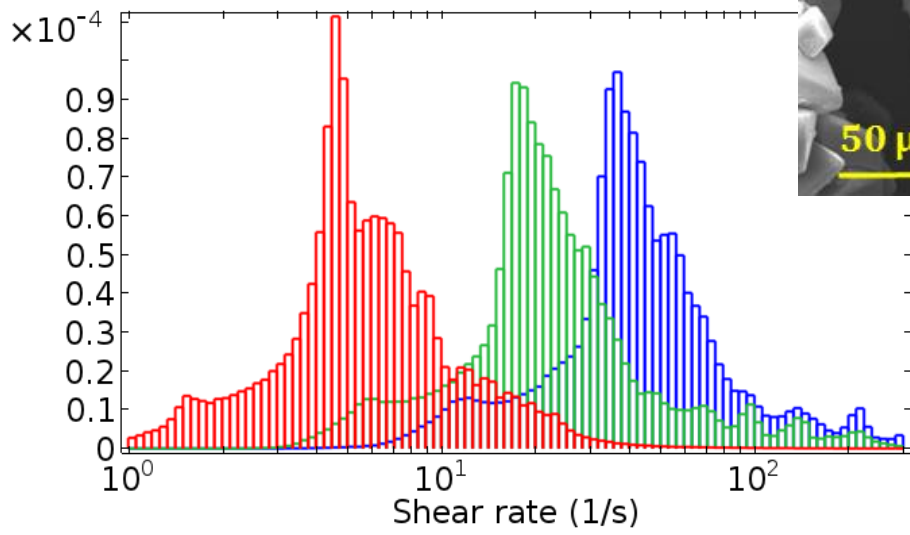
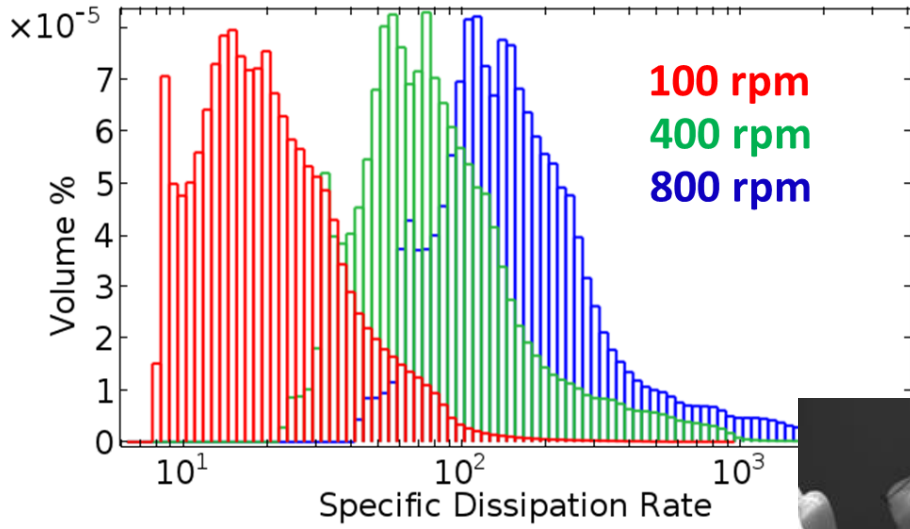


\* Rate at which turbulent energy converts to thermal internal energy

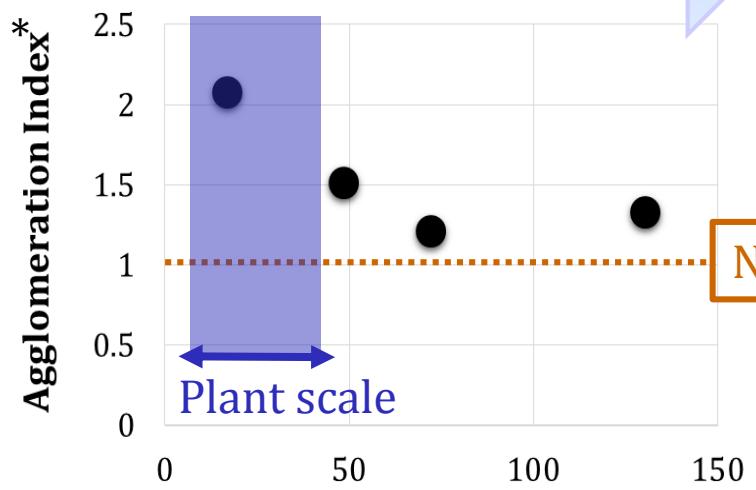
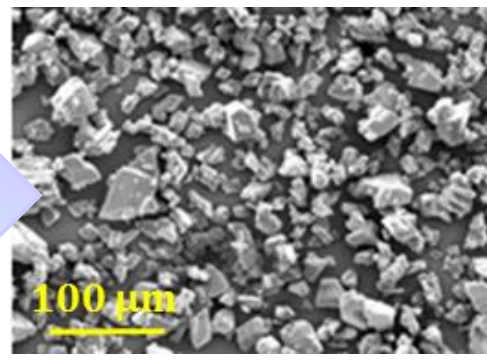
# Shear Rate Correlates with Particle Size and Agglomeration Index

**Next Step:** Extension of COMSOL modeling to the plant reactors to explore the studied correlations at scale and to predict the particle size at manufacturing scale

**Initial analysis:** Low shear rate at plant scale – risk of agglomeration



Particle attrition, breakage and de-agglomeration



No agglomeration

\* Represents the extent of agglomeration

# Summary

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- ◆ High shear rate enhances de-agglomeration and particle breakage, reducing particle size and agglomeration index.
- ◆ COMSOL is helpful in estimating the mixing attributes that can be used to predict the crystallization process behavior and final drug substance particle properties.



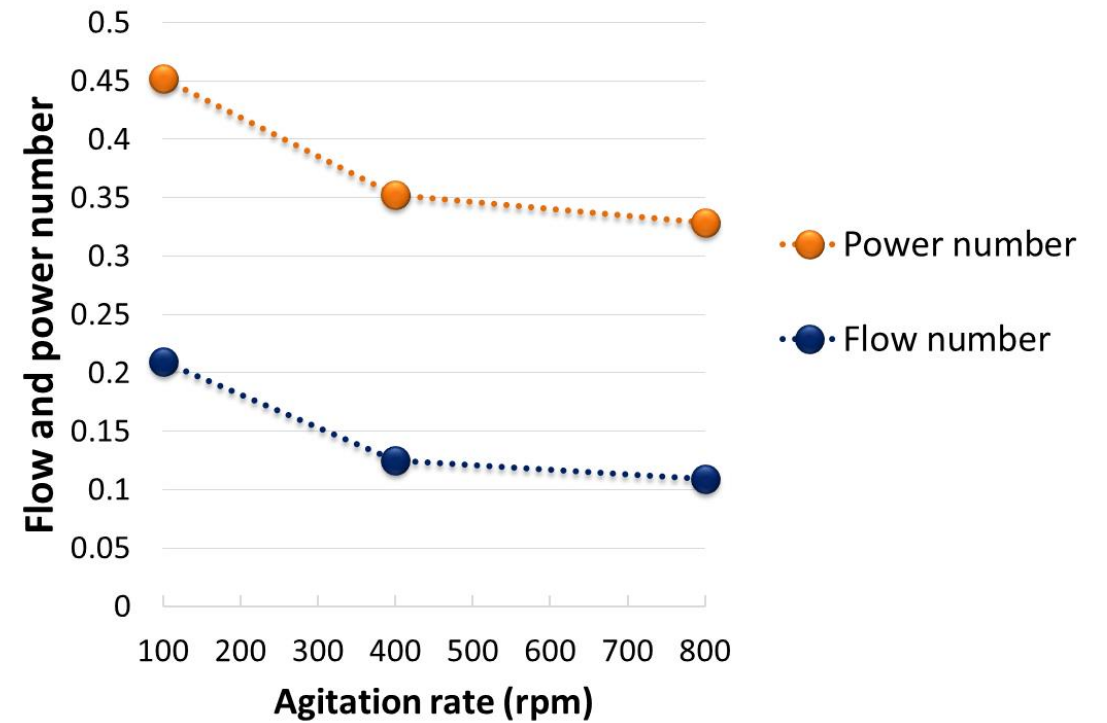
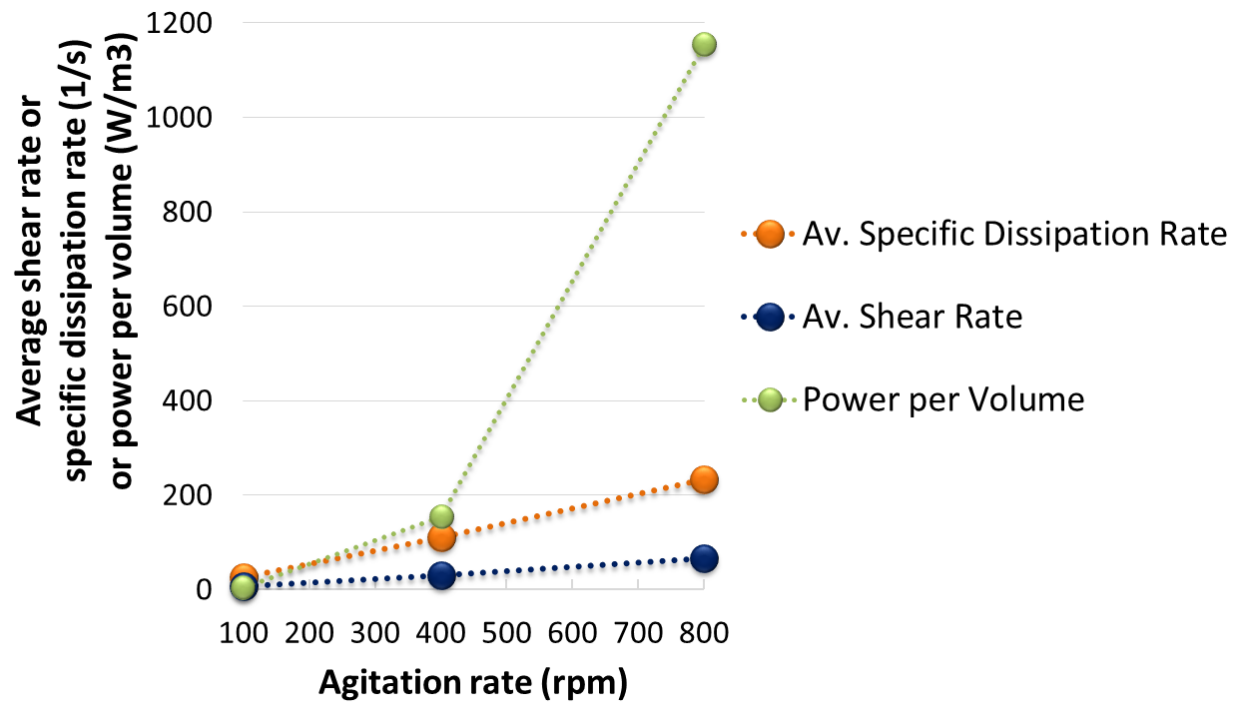
**THANK YOU FOR YOUR ATTENTION!**

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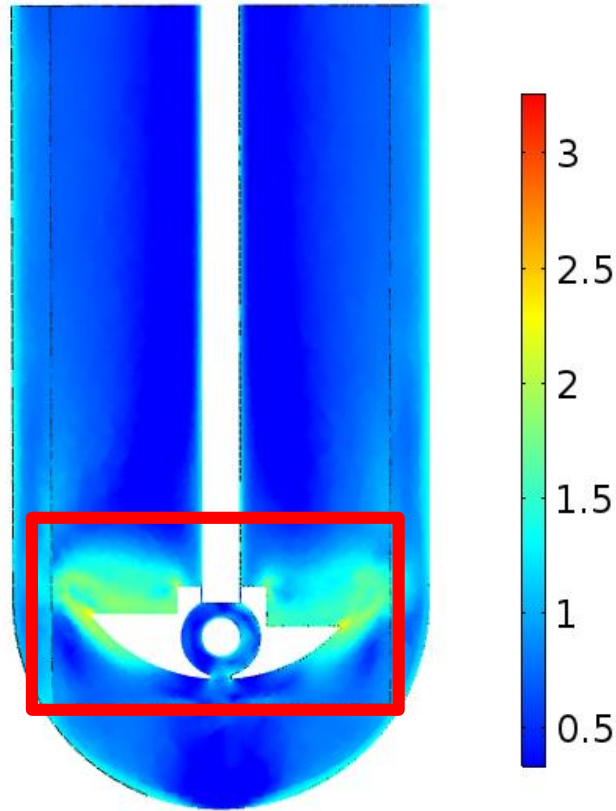


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# BACK-UP SLIDES



# Correlation at Scale-up



High shear zone-to-Total Volume ratio

4L Lab reactor = 0.18

1L Lab Reactor = 0.11

