

Topology Optimization for Liquid Cooled Heat Sink Design

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TopOPt for heat sink design



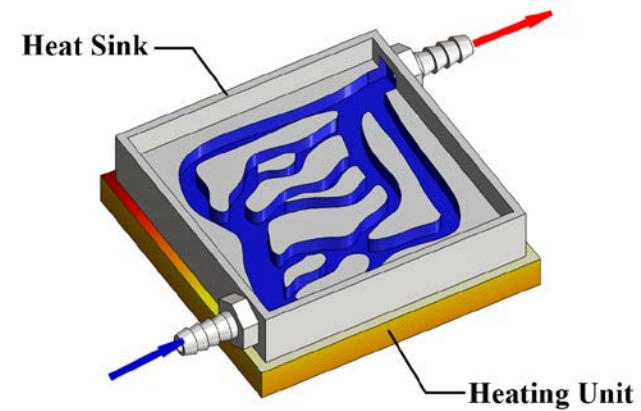
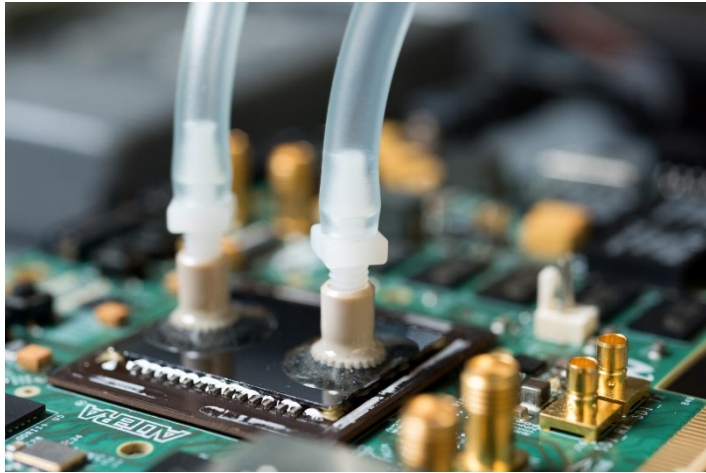
Passive cooling devices (natural convection)



TopOPt for heat sink design



Active cooling devices (forced convection)



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TopOPt for heat sink design



Common in TopOPt for heat sink design:

- Thermo-fluidic problems
- High nonlinear
- Topology (layout) determines the response of structure

We need to find the OPTIMAL TOPOLOGY (LAYOUT) to enhance the heat transfer rate.

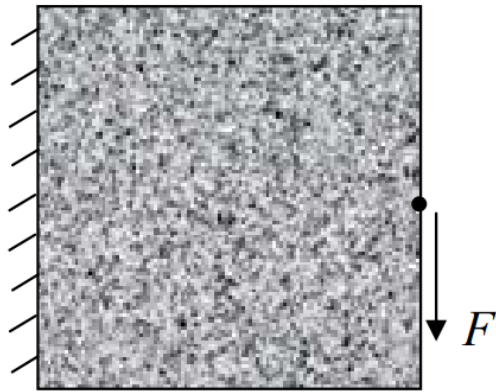


Our project use TOPOLOGY OPTIMIZATION to come up with the optimal cooling channel layout.

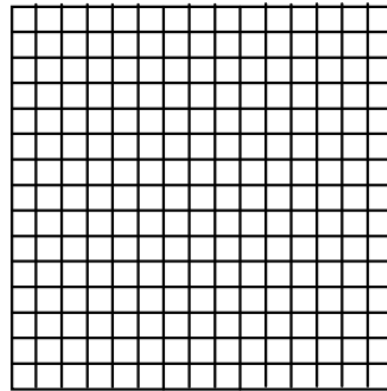
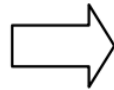
Structural Topology Optimization



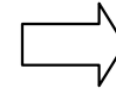
Bendsoe (1989), Zhou and Rozvany (1991), Miejski (1992)



Design problem



Discretized elements



Optimal topology

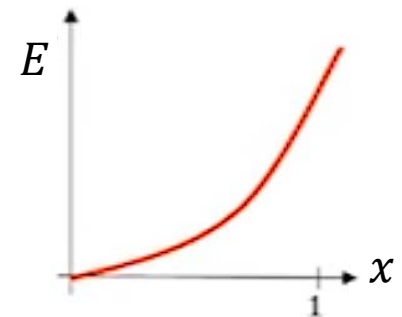
$$\text{Find : } X = \{x^1, x^2, \dots, x^N\}^T \quad (x_{\min} \leq x \leq x_{\max} = 1)$$

$$\text{Min : } C = F^T U = U^T K U$$

$$\text{s.t. : } V = f V_0 = \sum_{e=1}^N x^e v^e$$

$$F = K U$$

Interpolation function:



$$E(x_e) = x_e^p E_0$$

$$p > 1$$

Topology optimization



Common in TopOpt:

- Objective function
i.e. compliance, flow dissipation, sound pressure
- Design variable
- Constraint
i.e. volume fraction



Fluid problems

Navier-Stokes equations



Incompressible Navier-Stokes equation for porous flow

$$(\mathbf{u}^* \cdot \nabla^*) \mathbf{u}^* = \nabla^* \left[-p^* \mathbf{I} + \frac{1}{\text{Re}} \left(\nabla^* \mathbf{u}^* + (\nabla^* \mathbf{u}^*)^T \right) \right] - \alpha^* \mathbf{u}^*$$

$$\nabla^* \cdot \mathbf{u}^* = 0$$

Non-fluid (solid) domain

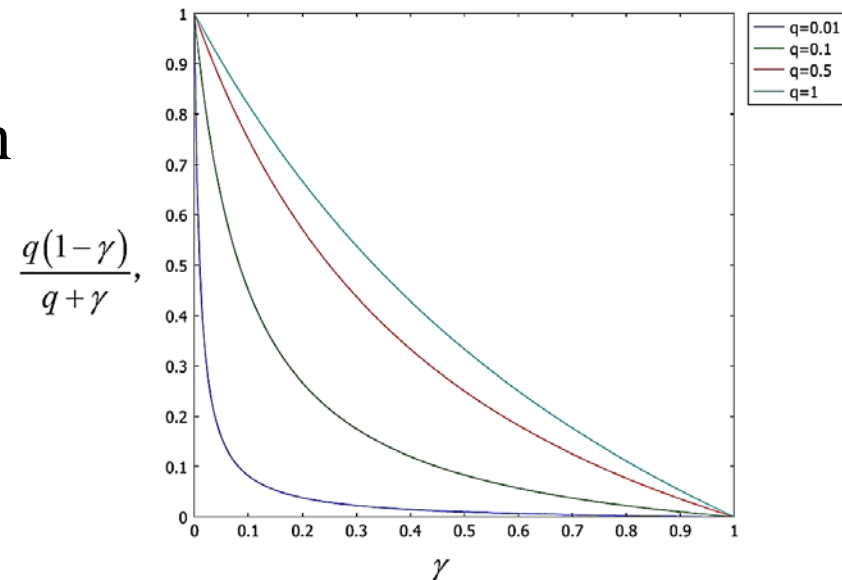
$$\gamma=0, \alpha \rightarrow \infty, F \rightarrow \infty \implies \mathbf{u}=0$$

Fluid domain

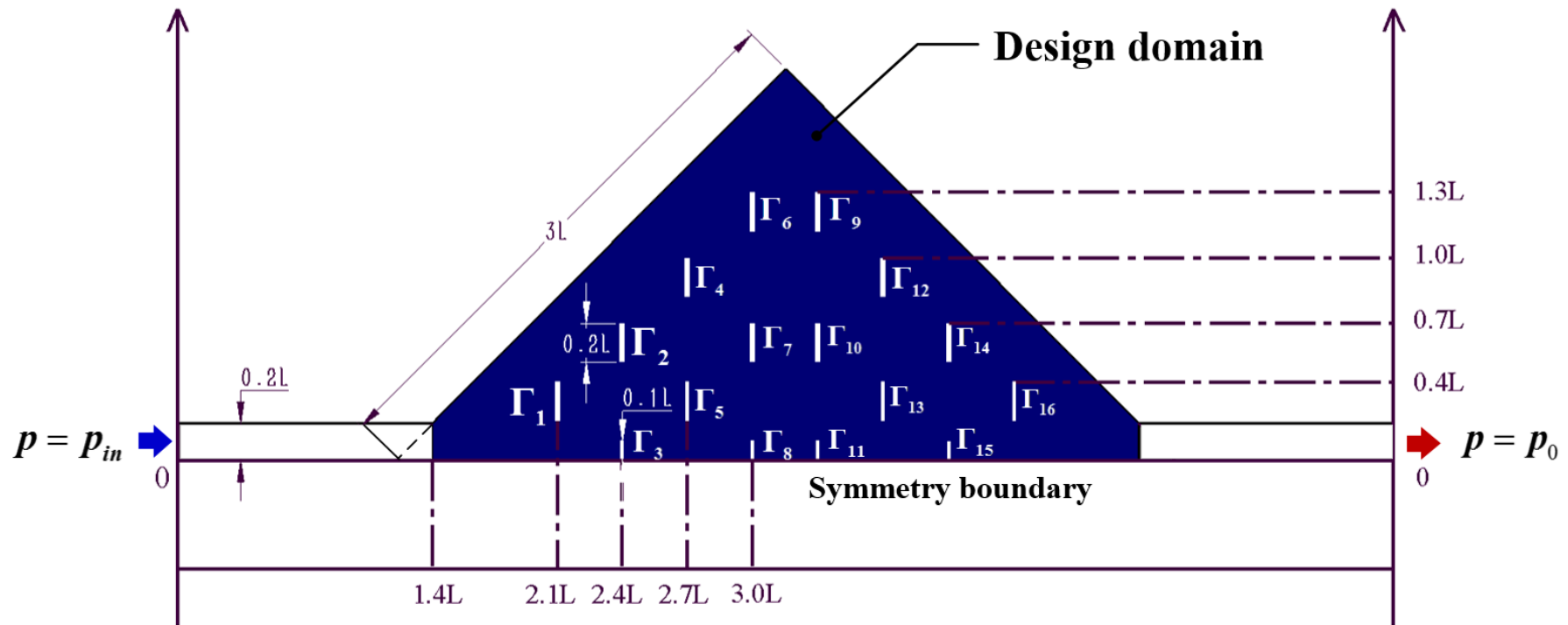
$$\gamma=1, \alpha \rightarrow 0, F \rightarrow 0 \implies \text{NS equation}$$

Interpolation function

$$\alpha^*(x) = \alpha_{\max}^* \frac{q(1-\gamma)}{q+\gamma}$$



2D flow distribution problem



$$\text{minimize}_{\gamma \in [0,1]} \Phi = \int_{\Omega} \left[\nabla^* \mathbf{u}^* \cdot (\nabla^* \mathbf{u}^* + \nabla^* \mathbf{u}^{*T}) + \alpha^* \mathbf{u}^* \cdot \mathbf{u}^* \right] d\Omega,$$

$$\text{s.t.} \quad \int_{\Omega} \gamma d\Omega \leq V_f \cdot \text{Vol}_{\Omega},$$

$$\int_{\Gamma_i} \mathbf{u}^* \cdot \mathbf{n} d\Gamma_i = FR_i \cdot \dot{V}_{in}, \quad i=1, \dots, n,$$

$$\int_{\Gamma_{in}} p_{in}^* u^* d\Gamma = 1,$$

$$FR_1 = FR_{16} = 1/2,$$

$$FR_2 = FR_{14} = 1/3,$$

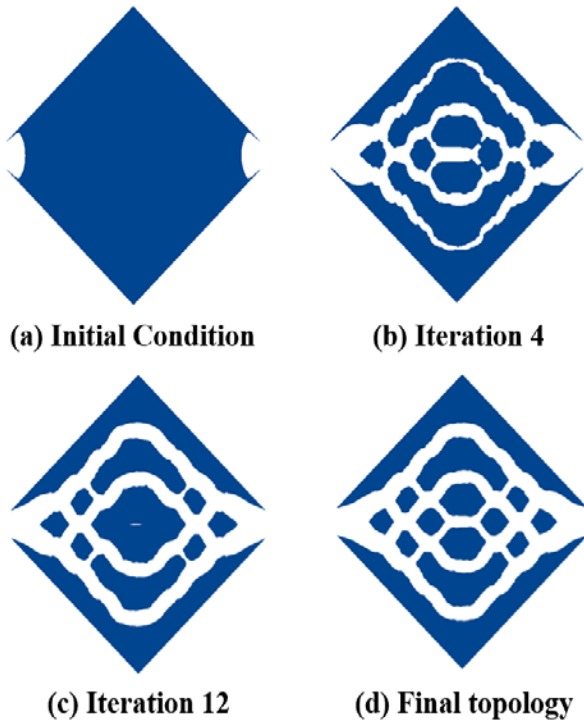
$$FR_3 = FR_{15} = 1/6,$$

$$FR_4 = FR_5 = FR_{12} = FR_{13} = 1/4,$$

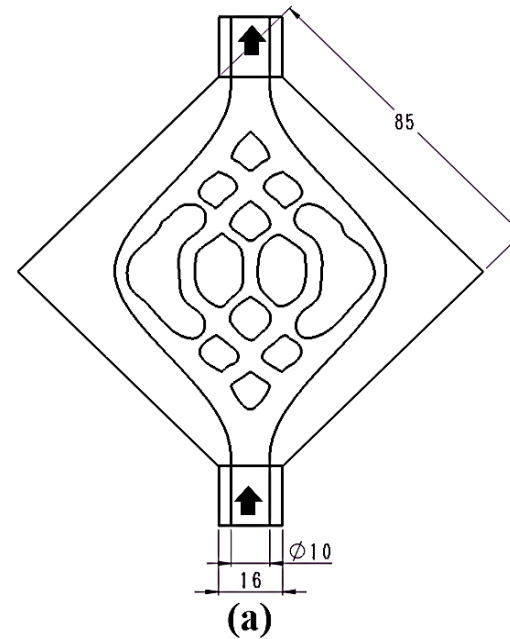
$$FR_6 = FR_7 = FR_9 = FR_{10} = 1/5,$$

$$FR_8 = FR_{11} = 1/10$$

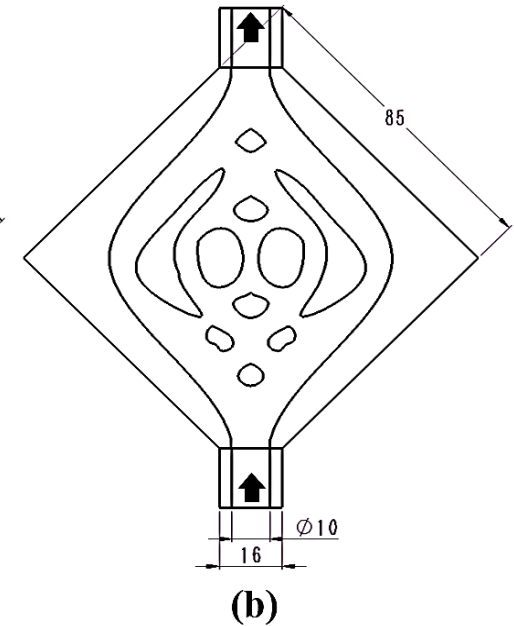
2D flow distribution problem



$V_f=40\%$



$V_f=60\%$



Iterative process
($V_f=40\%$)

Optimal channel layout



Thermo-fluidic problems

Navier-Stokes equations



Incompressible Navier-Stokes equation for porous flow

$$(\mathbf{u}^* \cdot \nabla^*) \mathbf{u}^* = \nabla^* \left[-p^* \mathbf{I} + \frac{1}{\text{Re}} \left(\nabla^* \mathbf{u}^* + (\nabla^* \mathbf{u}^*)^T \right) \right] - \alpha^* \mathbf{u}^*$$

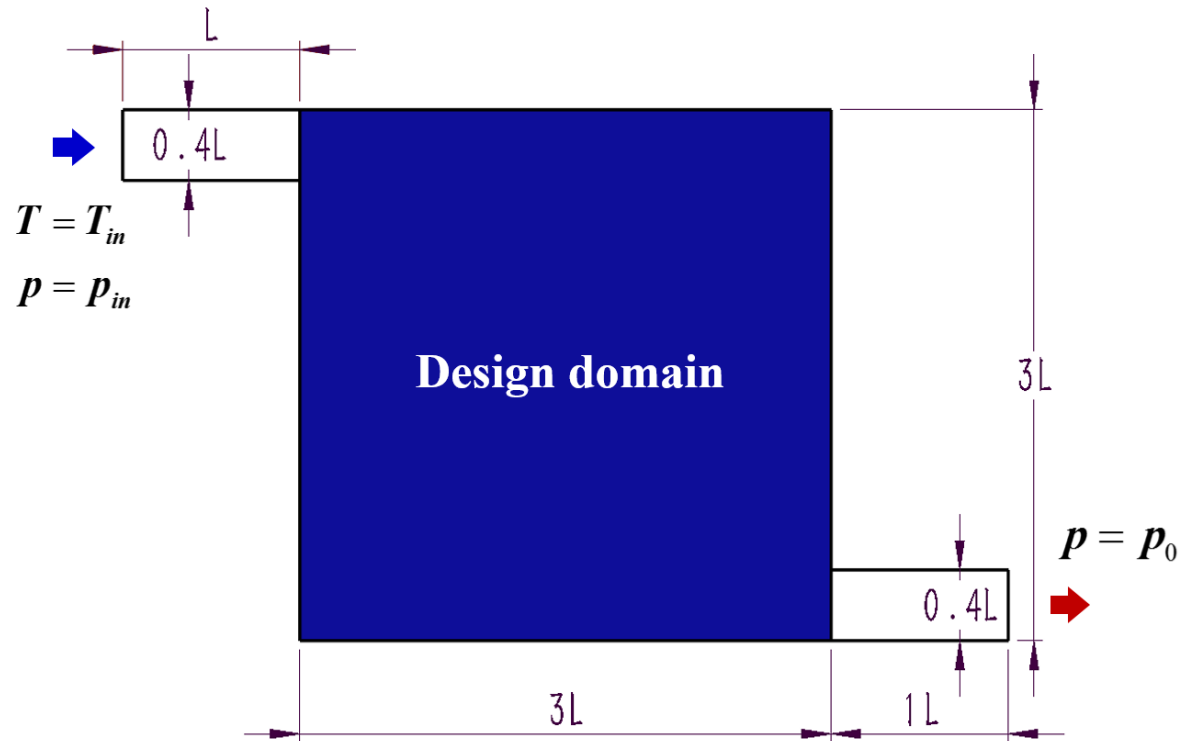
$$\nabla^* \cdot \mathbf{u}^* = 0$$

Energy equation

$$\text{Re Pr} (\mathbf{u}^* \cdot \nabla^*) T^* = \nabla^{*2} T^*, \quad (\text{in fluid domains})$$

$$0 = \nabla^{*2} T^* + Q^*, \quad (\text{in solid domains})$$

2D heat exchange problem



$$\text{maximize}_{\gamma \in [0,1]} \Phi = \int_{\Omega} (1-\gamma) h^* (1-T^*) d\Omega,$$

$$\text{s.t.} \quad \int_{\Omega} \gamma d\Omega \leq V_f \cdot \text{Vol}_{\Omega},$$

$$\int_{\Gamma_{in}} p_{in}^* u^* d\Gamma = 1.$$

2D heat exchange problem



(a) Initial Condition



(b) Iteration 5

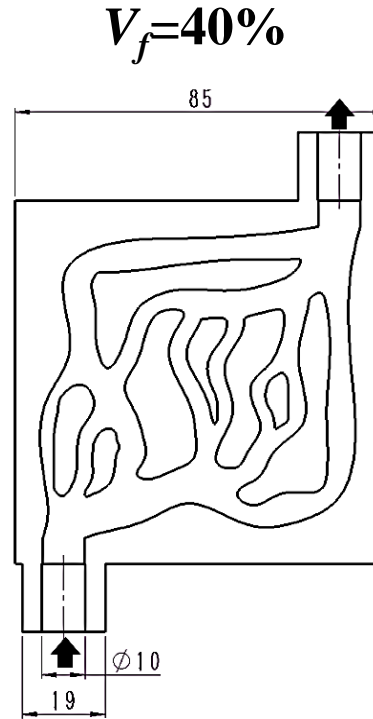


(c) Iteration 17

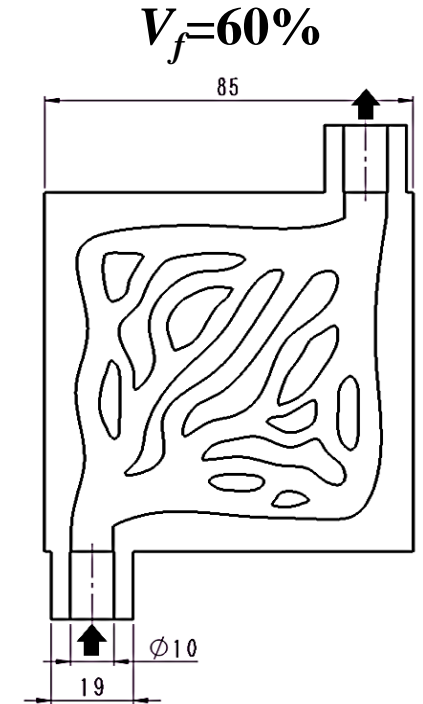


(d) Final topology

Iterative process
($V_f=40\%$)



(a)



(b)

Optimal channel layout

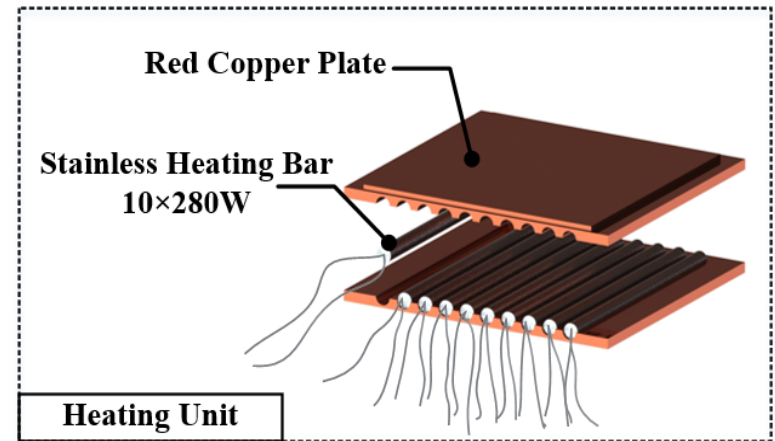
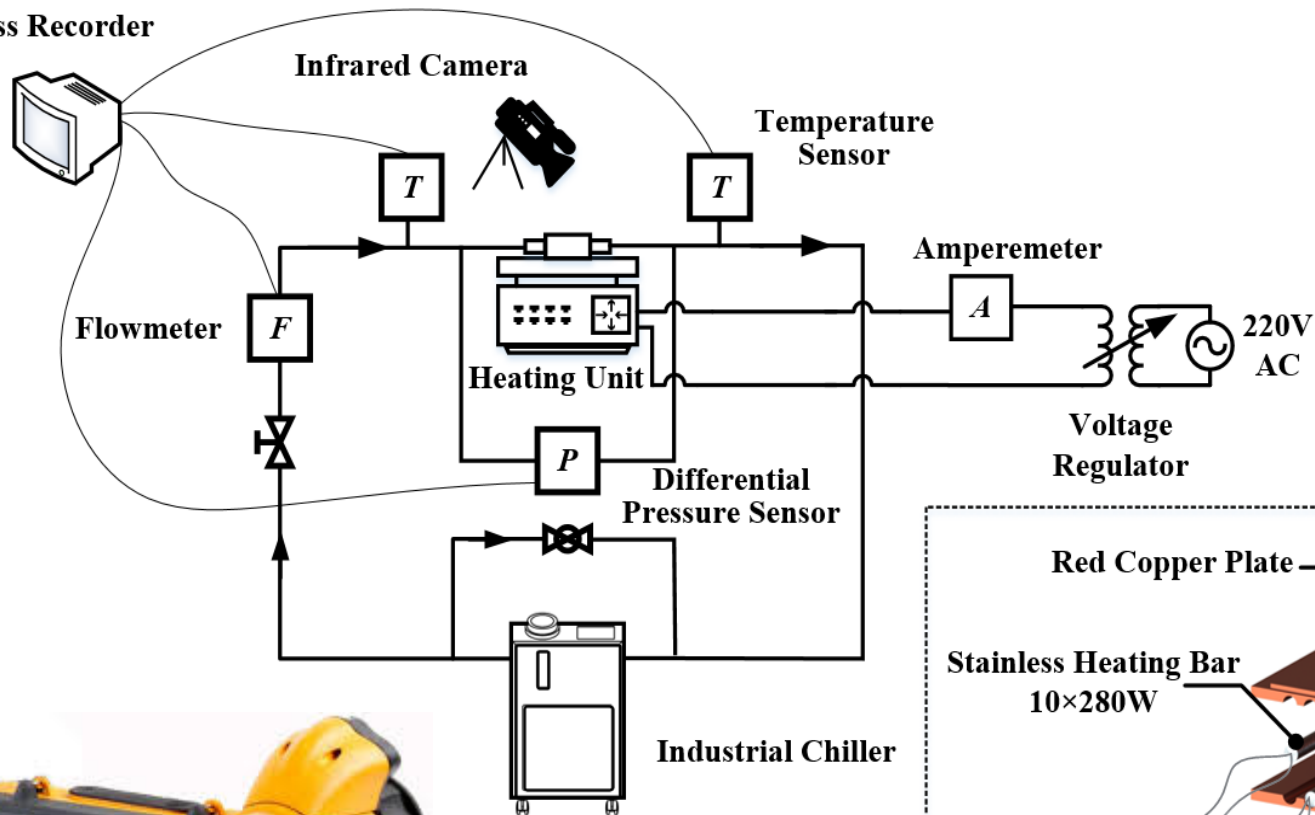


Flow and Thermal Performance

Experimental Verification



Paperless Recorder



Reference case



Channel Layout

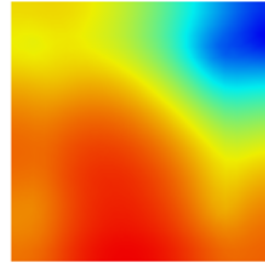
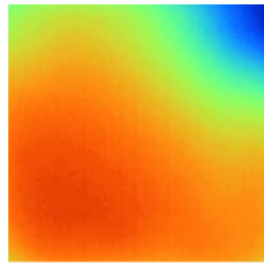
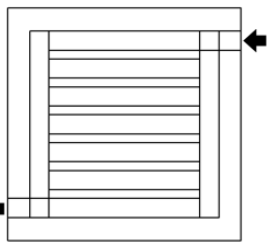
Experimental Study

Numerical Study

Experimental Study

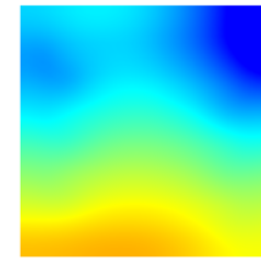
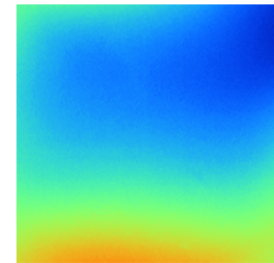
Numerical Study

Channel Layout




$\Delta p = 200 \text{ Pa}$, $V_f = 0.4$

(a)

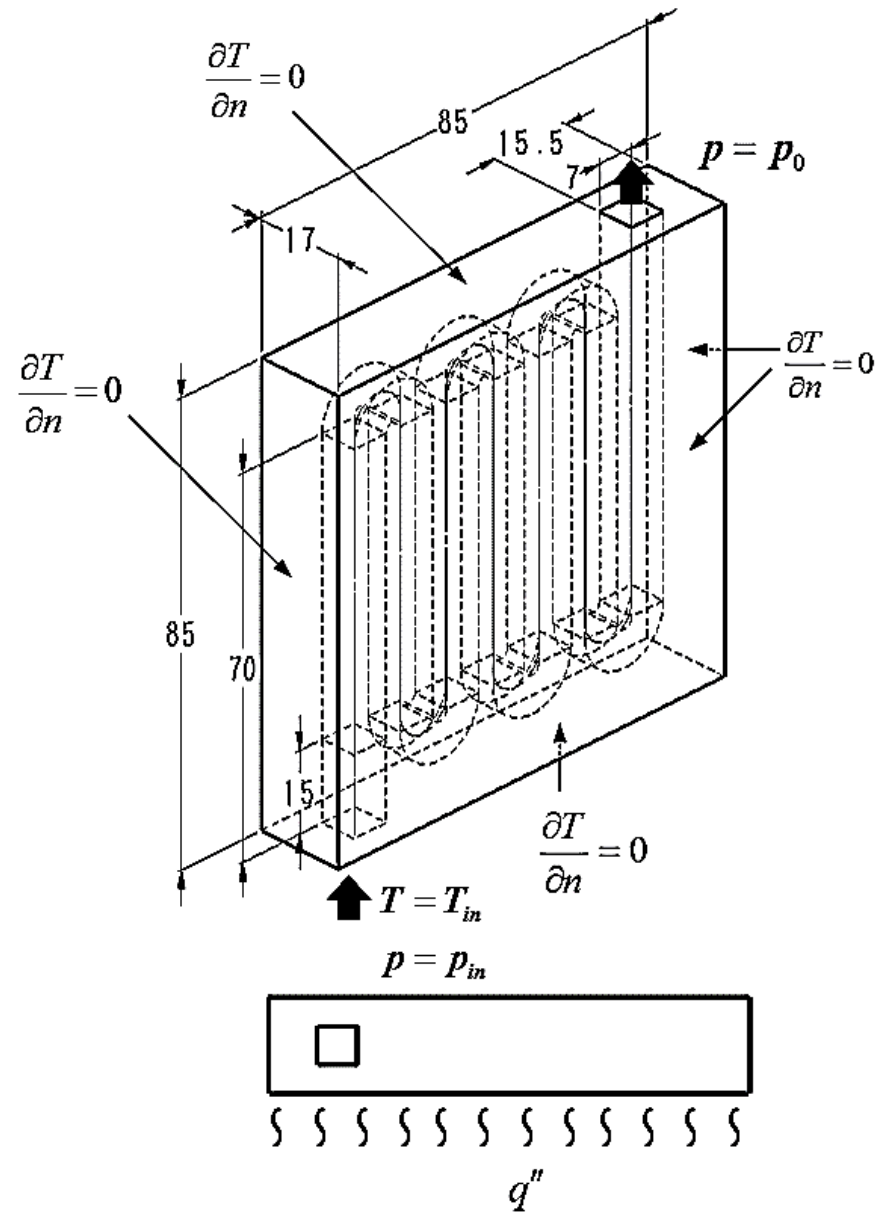


$\Delta p = 200 \text{ Pa}$, $V_f = 0.4$

(b)

31.1[°C]  58.8[°C]

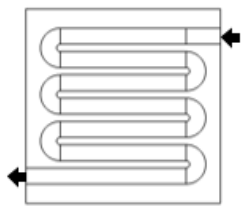
Reference case



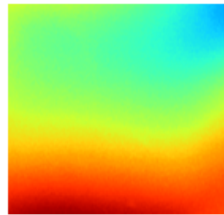
Temp. distrib. (Exper. VS Numerical)



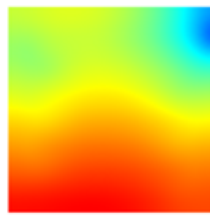
Channel Layout



Experimental Study

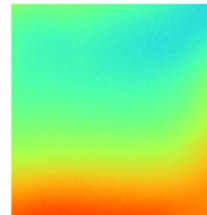


Numerical Study

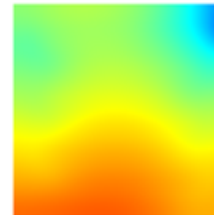


$\Delta p = 200 \text{ Pa}$, $V_f = 0.4$

Experimental Study

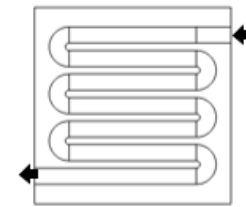


Numerical Study



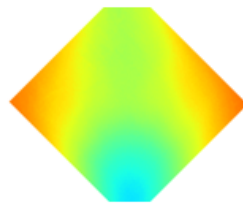
$\Delta p = 200 \text{ Pa}$, $V_f = 0.6$

Channel Layout



(a)

Experimental Study

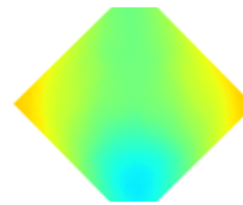


Numerical Study

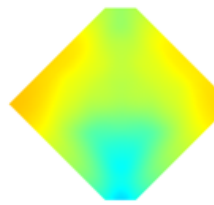


$\Delta p = 200 \text{ Pa}$, $V_f = 0.4$

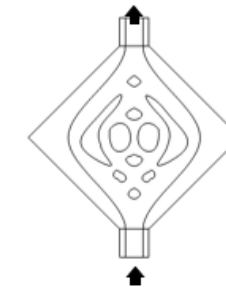
Experimental Study



Numerical Study

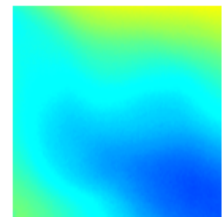


$\Delta p = 200 \text{ Pa}$, $V_f = 0.6$

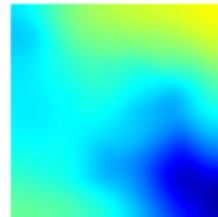


(b)

Experimental Study

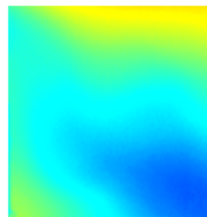


Numerical Study

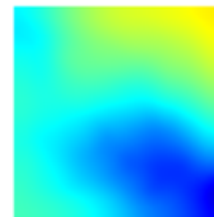


$\Delta p = 200 \text{ Pa}$, $V_f = 0.4$

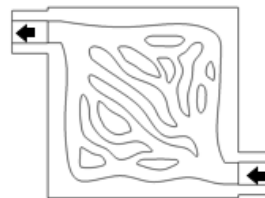
Experimental Study



Numerical Study



$\Delta p = 200 \text{ Pa}$, $V_f = 0.6$



(c)

27.9[°C] 53.2[°C]

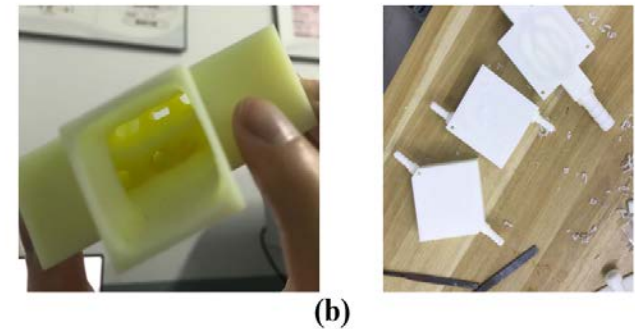
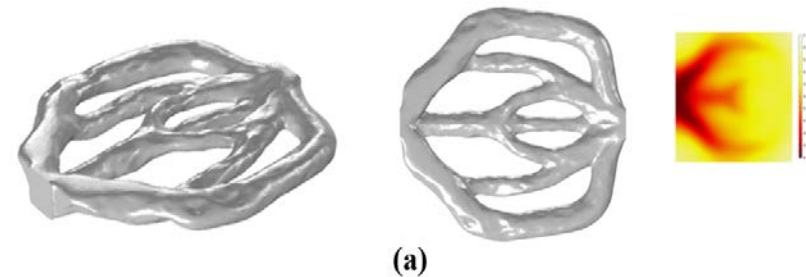
Conclusions



- Presented industrial application of TO in fluids, thermo-fluidic problems
- We are at the verge of being able to send TO results to manufacturing

Future works...

- 3D channels with 3DP technology
- TO considering turbulent flow





Thanks for your attention!

Q&A



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